



Constitutive model for the fluid-particle drag coefficient in filtered two-fluid models for gas-particle flows

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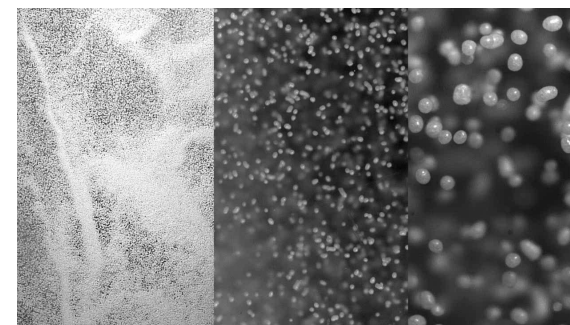
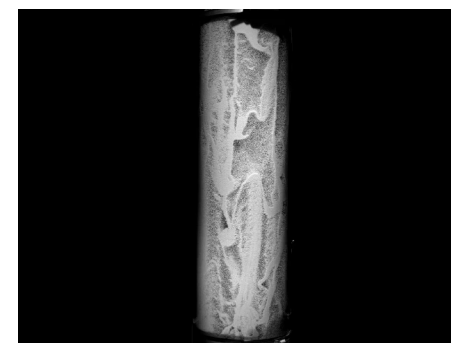
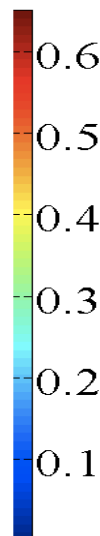
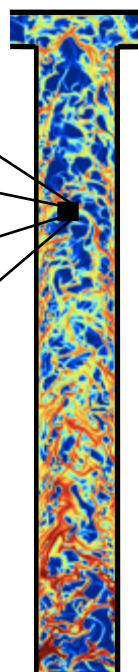
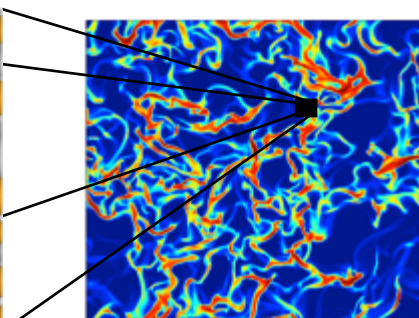
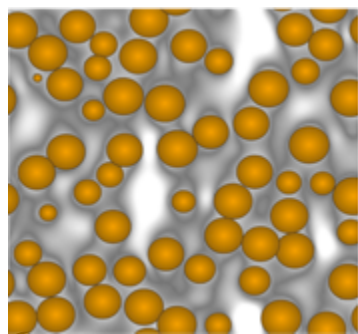


Filtered two-fluid model: Overview

MICRO-SCALE $\sim 50\mu\text{m}-\text{mm}$

MESO-SCALE $\sim \text{mm}-\text{cm}$

MACRO-SCALE $\sim \text{cm}-\text{m}$



DEM for particles,
DNS or CFD of
averaged equations
for the fluid flow.

Volume-averaged
hydrodynamic models for
fluid and particle phases.

Filtered volume-averaged
hydrodynamic models for
fluid and particle phases.

High Speed
Particle Imaging:
Riser Flow

Engineering need:
tools to probe macro-scale
flow features directly.

Filtered two-fluid model: Overview



Develop models that allow us to focus on large-scale flow structures, without ignoring the possible consequence of the smaller scale structures.

Original two-fluid model and constitutive relations

Significant advances in the past three decades



Filtered two-fluid model

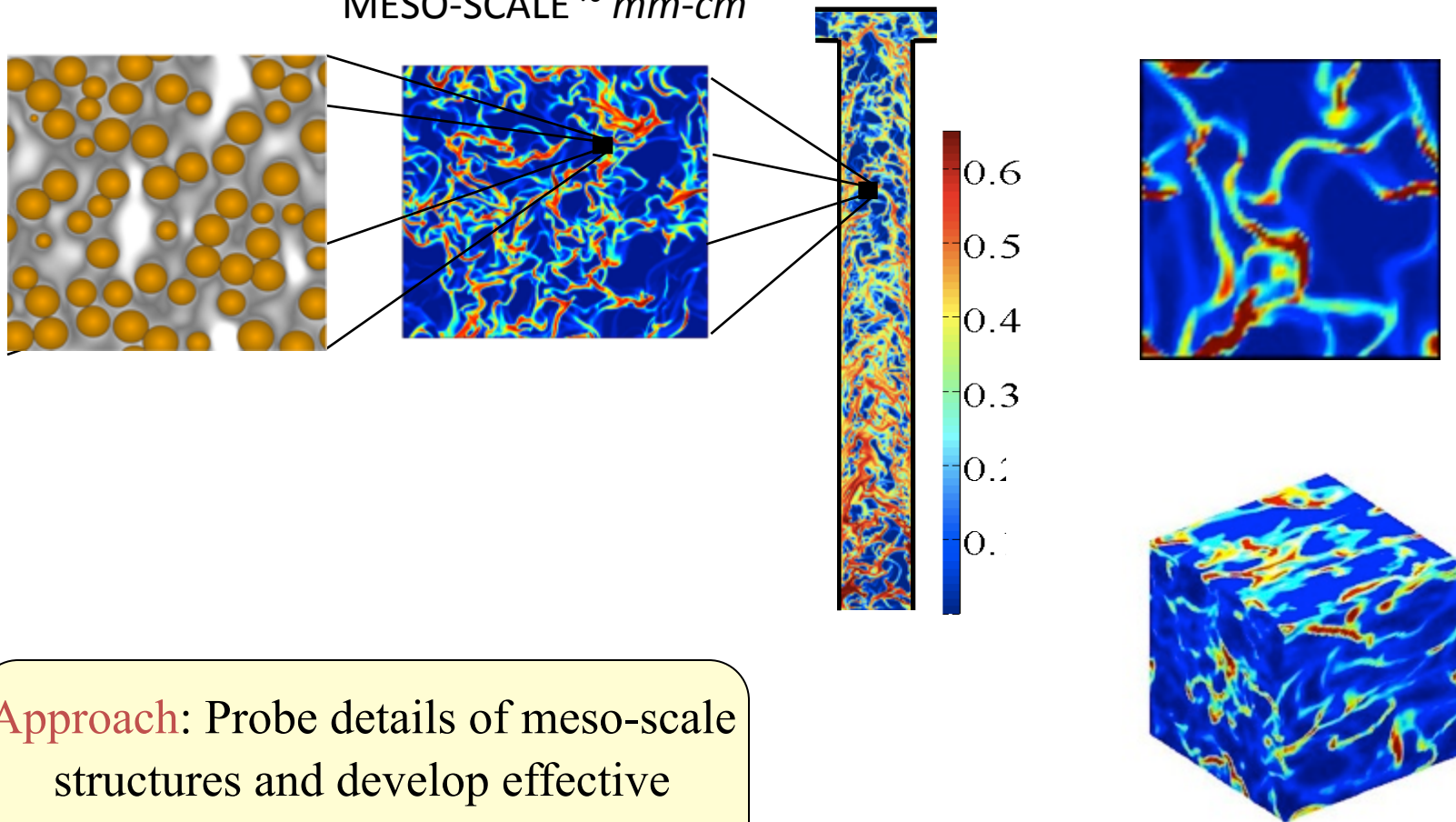
*Modified constitutive relations for hydrodynamic terms
species and energy dispersion*
interphase heat and mass transfer rates*
even modified reaction rate expressions!*

Filtered two-fluid model: Overview

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MESO-SCALE $\sim \text{mm}-\text{cm}$

MACRO-SCALE $\sim \text{cm}-\text{m}$



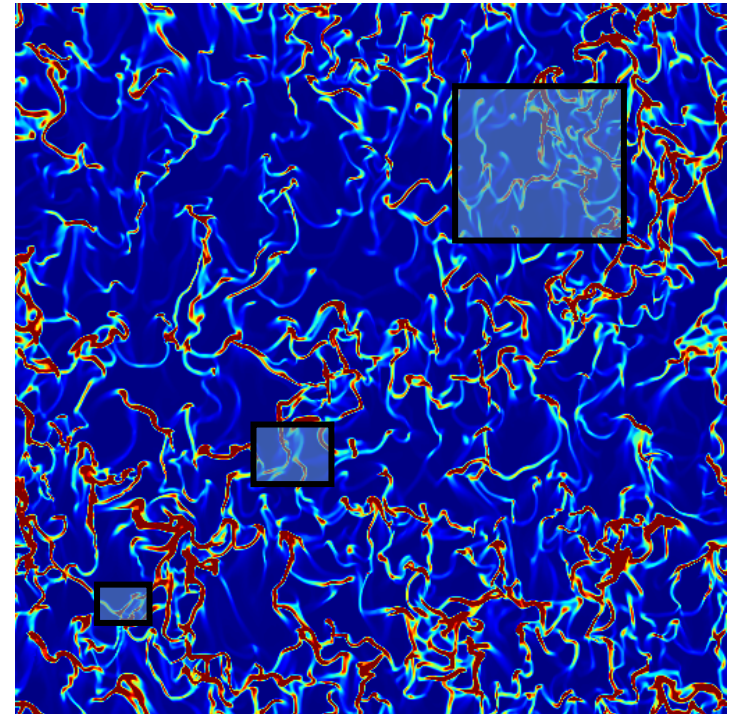
Approach: Probe details of meso-scale structures and develop effective coarse-grained equations

Filtered two-fluid model: Overview

Filter “data” generated through highly resolved simulations of two-fluid models

- ◆ Snapshot of particle volume fraction field – **kinetic theory** based two-fluid model.
- ◆ Squares of different sizes illustrate **regions (i.e. filters)** of different sizes.

$$\tilde{\mathbf{V}}_g = \frac{\overline{\phi_g \mathbf{V}_g}}{\phi_g}; \quad \tilde{\mathbf{V}}_s = \frac{\overline{\phi_s \mathbf{V}_s}}{\phi_s}$$



$$\Delta_{grid} \ll \Delta_{fil} \ll \Delta_{domain}$$

Filtered drag coefficient

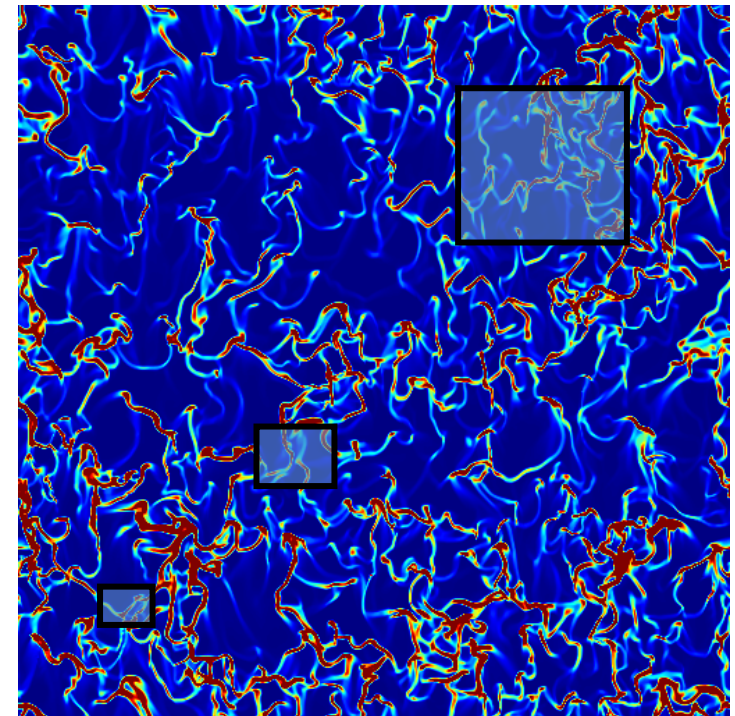
Filter “data” generated through highly resolved simulations of two-fluid models

- ◆ Snapshot of particle volume fraction field – **kinetic theory** based two-fluid model.
- ◆ Squares of different sizes illustrate **regions (i.e. filters)** of different sizes.

β_{fil} = filtered drag coefficient

$$\beta_{micro} \left(\phi_s, \left| \mathbf{v}_g - \mathbf{v}_s \right| \right) \left(v_{gy} - v_{sy} \right) - \phi'_s \frac{\partial p'_g}{\partial y}$$

$$= \frac{\left(\tilde{v}_{gy} - \tilde{v}_{sy} \right)}{\left(\tilde{v}_{gy} - \tilde{v}_{sy} \right)}$$



$$\Delta_{grid} \ll \Delta_{fil} \ll \Delta_{domain}$$

Filtered drag coefficient

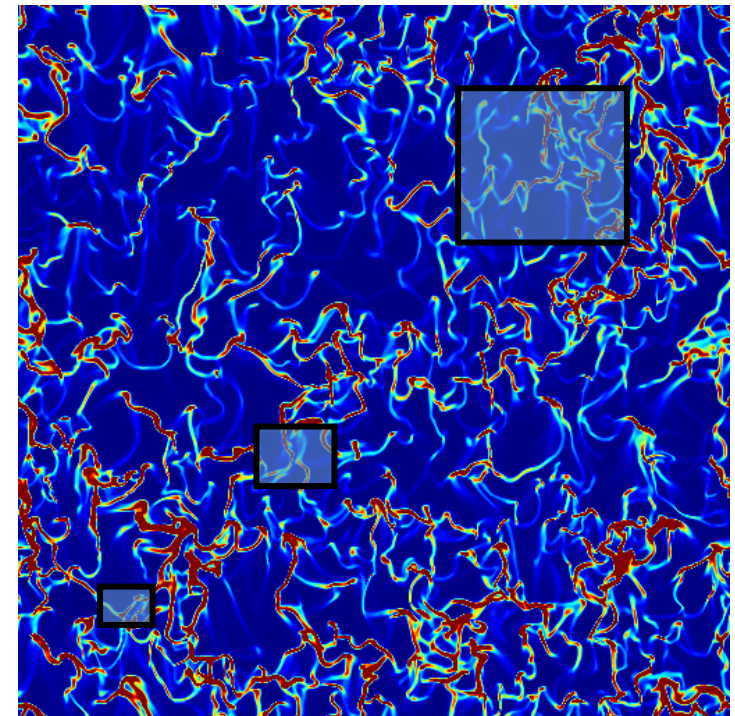
Filter “data” generated through highly resolved simulations of two-fluid models

- ◆ Snapshot of particle volume fraction field – **kinetic theory** based two-fluid model.
- ◆ Squares of different sizes illustrate **regions (i.e. filters)** of different sizes.

$$\beta_{fil} = \text{filtered drag coefficient}$$

$$= \beta_{micro} \left(\bar{\phi}_s, \left| \tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s \right| \right) (1 - H)$$

$$H = f \left(\frac{g \Delta_{fil}}{V_t^2}, \underbrace{\dots}_{\text{parameters characterizing sub-filter scale structure}} \right)$$



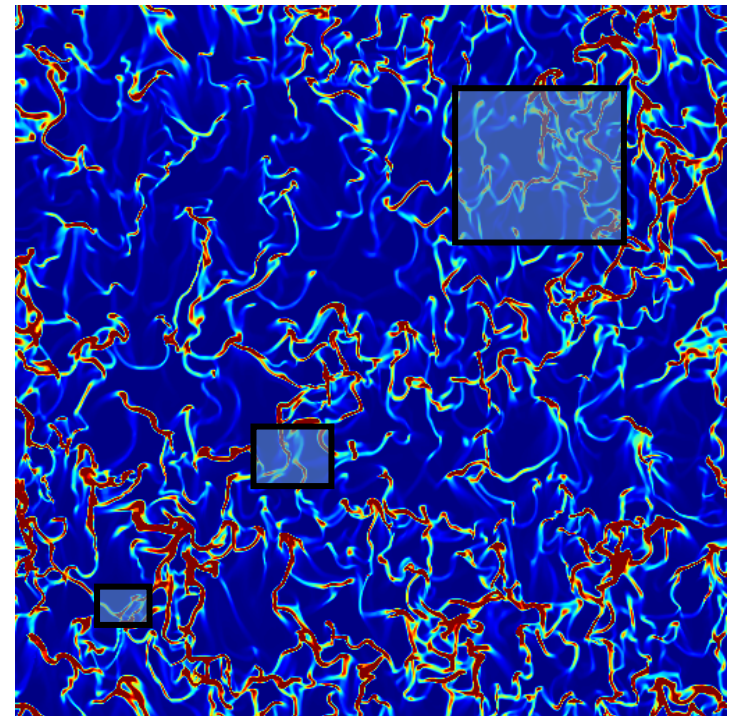
$$\Delta_{grid} \ll \Delta_{fil} \ll \Delta_{domain}$$

Filtered two-fluid model: Overview

Filter “data” generated through highly resolved simulations of two-fluid models

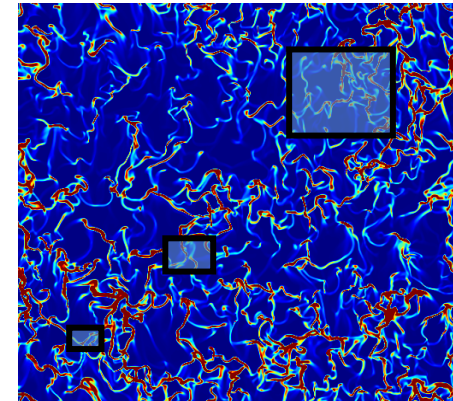
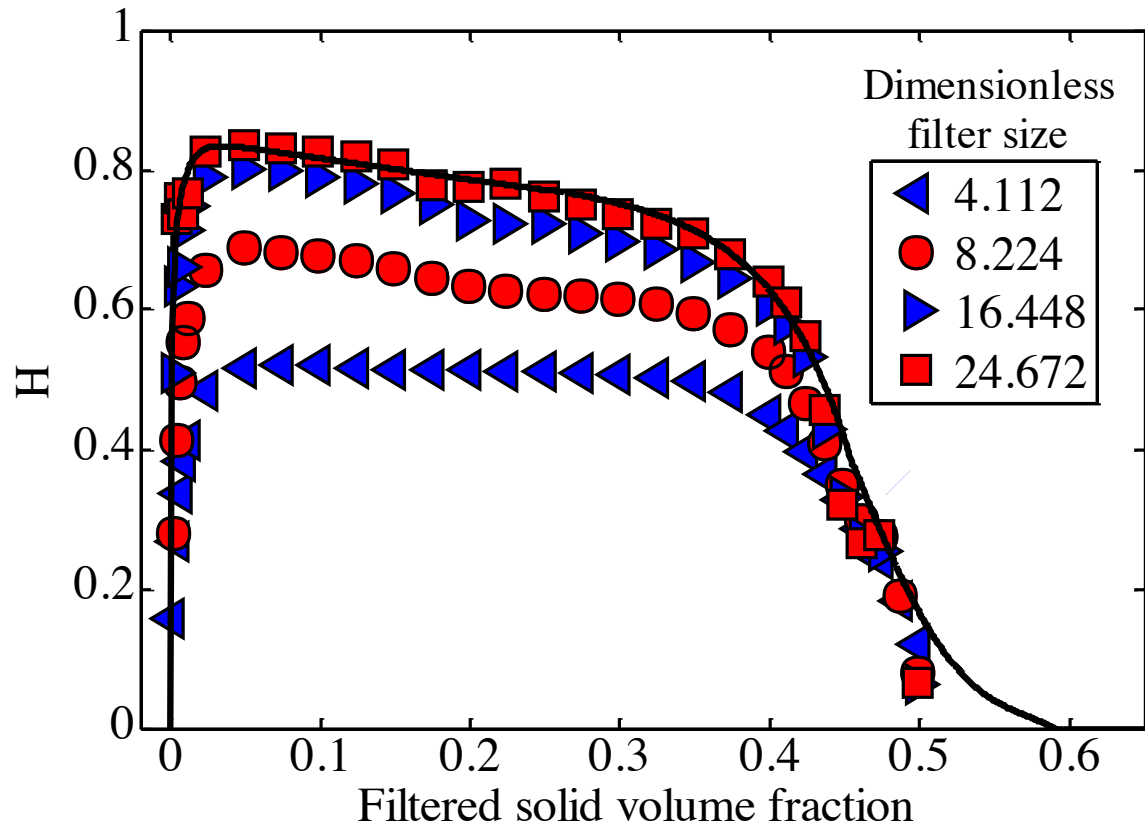
- ◆ Snapshot of particle volume fraction field – **kinetic theory** based two-fluid model.
- ◆ Squares of different sizes illustrate **regions (i.e. filters)** of different sizes.

$$\begin{aligned}\beta_{fil} &= \text{filtered drag coefficient} \\ &= \beta_{micro} \left(\bar{\phi}_s, \left| \tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s \right| \right) (1 - H) \\ H &= f \left(\frac{g \Delta_{fil}}{v_t^2}, \bar{\phi}_s \right)\end{aligned}$$



$$\Delta_{grid} \ll \Delta_{fil} \ll \Delta_{domain}$$

Filtered drag coefficient



$\left\{ \begin{array}{l} 75 \mu m \text{ FCC particles} \\ \text{ambient air} \end{array} \right\}$

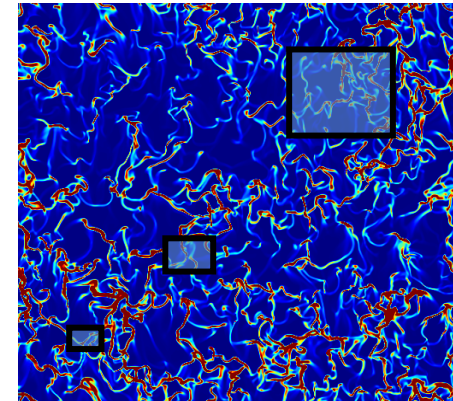
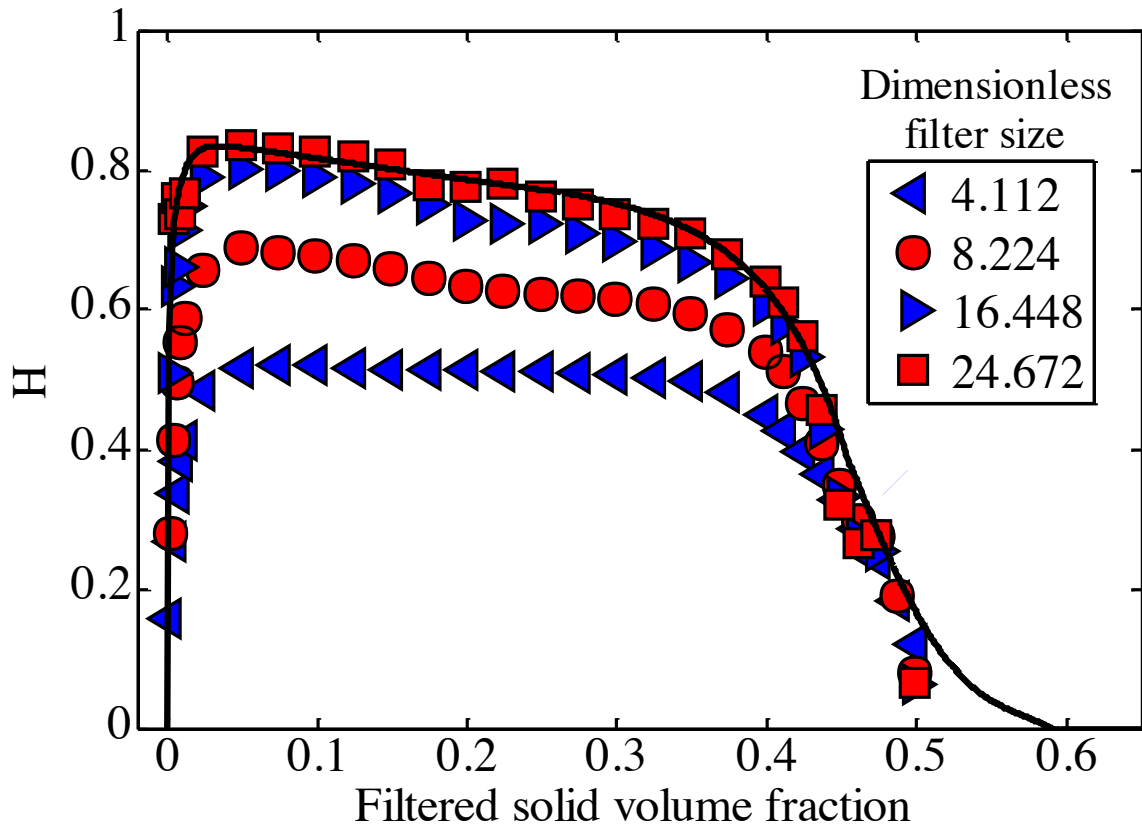
$$\frac{g \Delta_{fil}}{v_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1 \text{ cm}$$

$$\beta_{fil} = \beta_{micro} \left(\bar{\phi}_s, \left| \tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s \right| \right) (1 - H);$$

$$H = f \left(\frac{g \Delta_{fil}}{v_t^2}, \bar{\phi}_s \right)$$

Igci et al., (2008, 2010, 2011a, 2011b)

Filtered drag coefficient: The present study



{ 75 μm FCC particles }
 { ambient air }

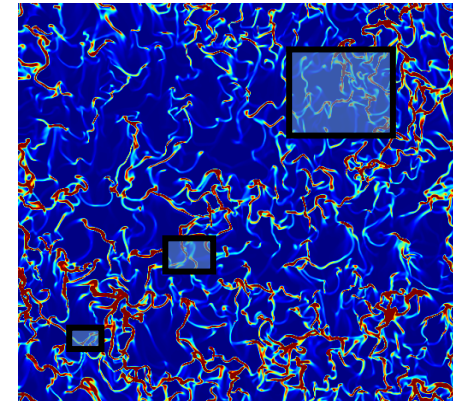
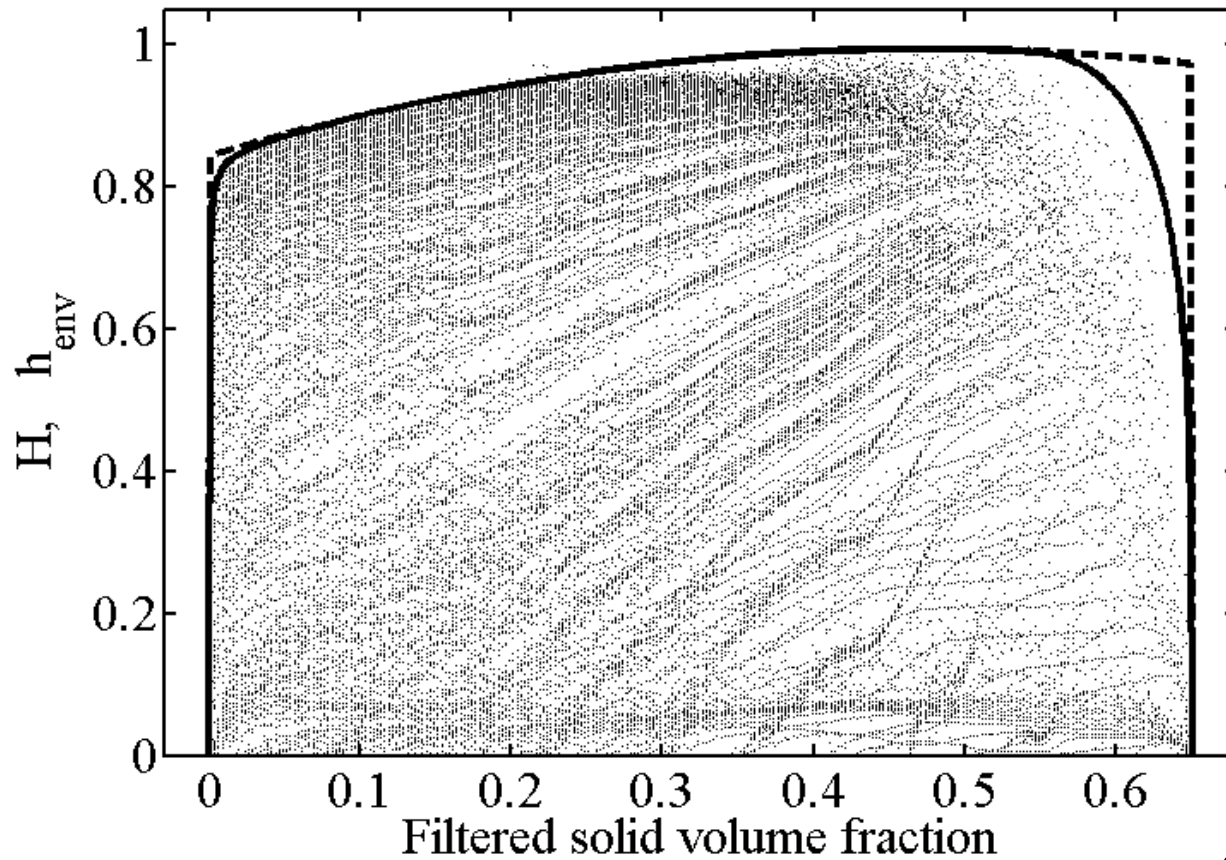
$$\frac{g\Delta_{fil}}{V_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1cm$$

$$\beta_{fil} = \beta_{micro}(\bar{\phi}_s, |\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|)(1 - H);$$

$$H = f\left(\frac{g\Delta_{fil}}{V_t^2}, \bar{\phi}_s, \underbrace{\dots}_{\text{parameters characterizing sub-filter scale structure}}\right)$$

Igci et al., (2008, 2010, 2011a, 2011b)

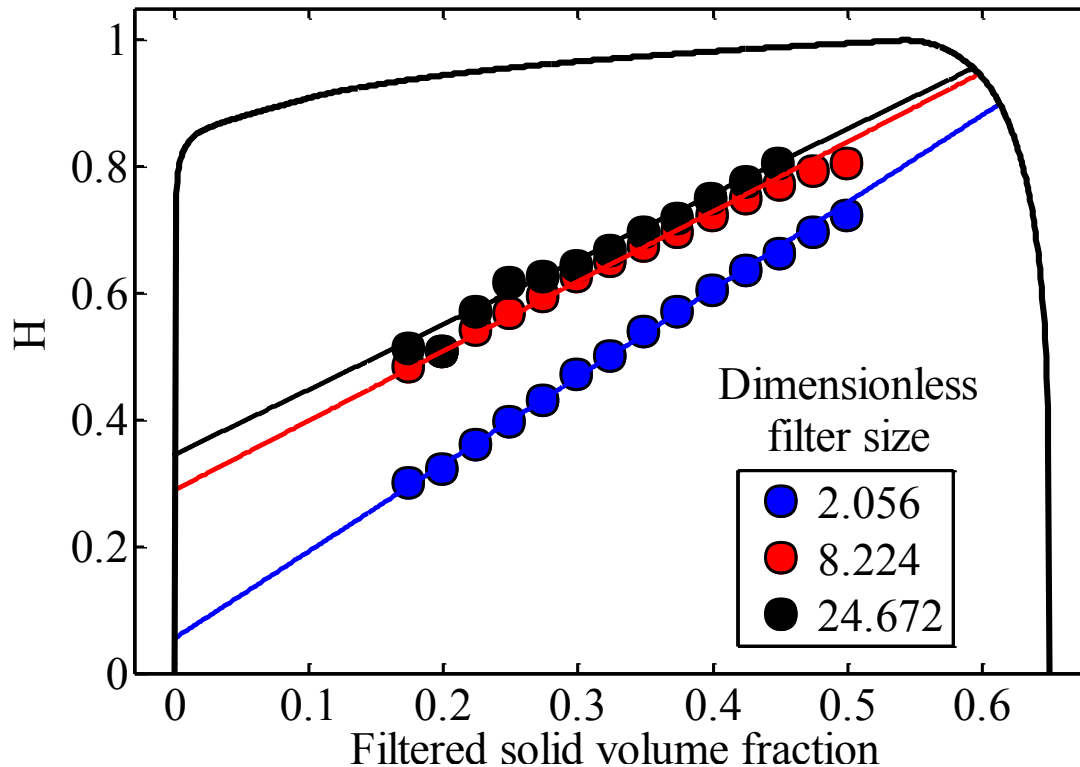
Filtered drag coefficient: The present study



$$\beta_{fil} = \beta_{micro}(\bar{\phi}_s, |\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|)(1 - H);$$

$$H = f\left(\frac{g\Delta_{fil}}{v_t^2}, \bar{\phi}_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{v_t}\right)$$

Filtered drag coefficient: The present study

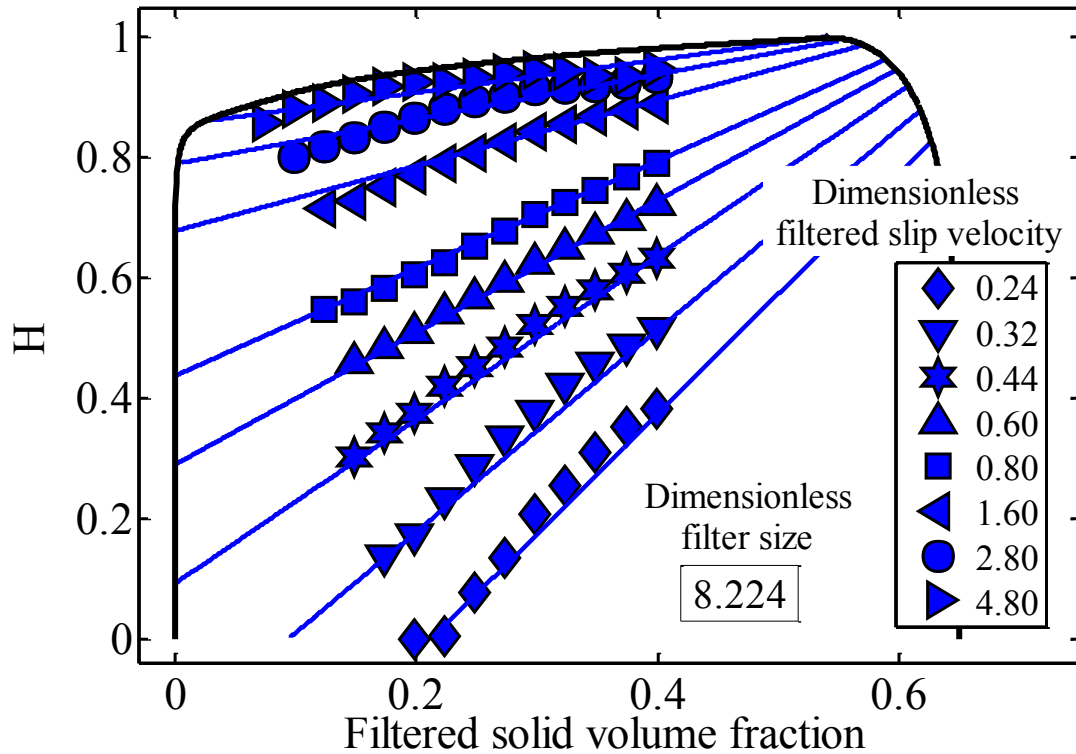


$$\frac{\langle |\tilde{\mathbf{v}}_{\text{slip}}| \rangle}{v_t} = 0.60$$

- As filter size increases, the filtered drag coefficient decreases.
- Does suggest the existence of large filter size asymptote.

$$H = f\left(\frac{g\Delta_{fil}}{v_t^2}, \bar{\phi}_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{v_t}\right) \left\{ \begin{array}{l} 75\mu\text{m FCC particles} \\ \text{ambient air} \end{array} \right\} \quad \frac{g\Delta_{fil}}{v_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1\text{cm}$$

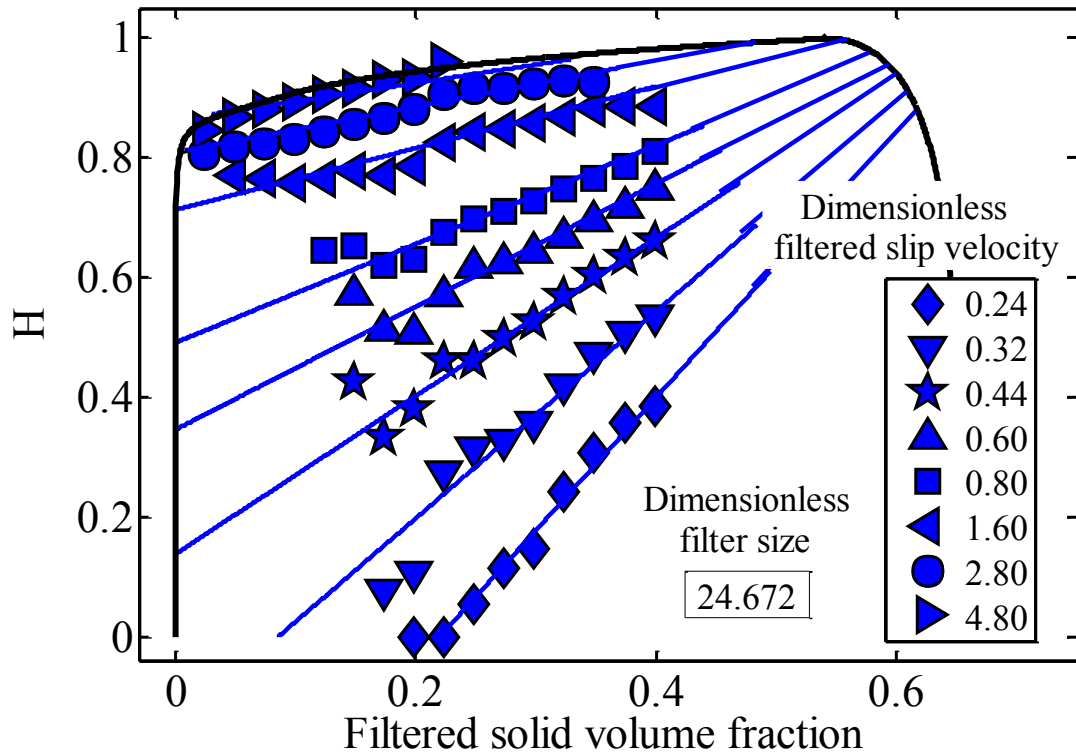
Filtered drag coefficient: The present study



- As slip velocity increases, the filtered drag coefficient decreases.

$$H = f\left(\frac{g\Delta_{fil}}{v_t^2}, \bar{\phi}_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{v_t}\right) \left\{ \begin{array}{l} 75\mu\text{m FCC particles} \\ \text{ambient air} \end{array} \right\} \quad \frac{g\Delta_{fil}}{v_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1\text{cm}$$

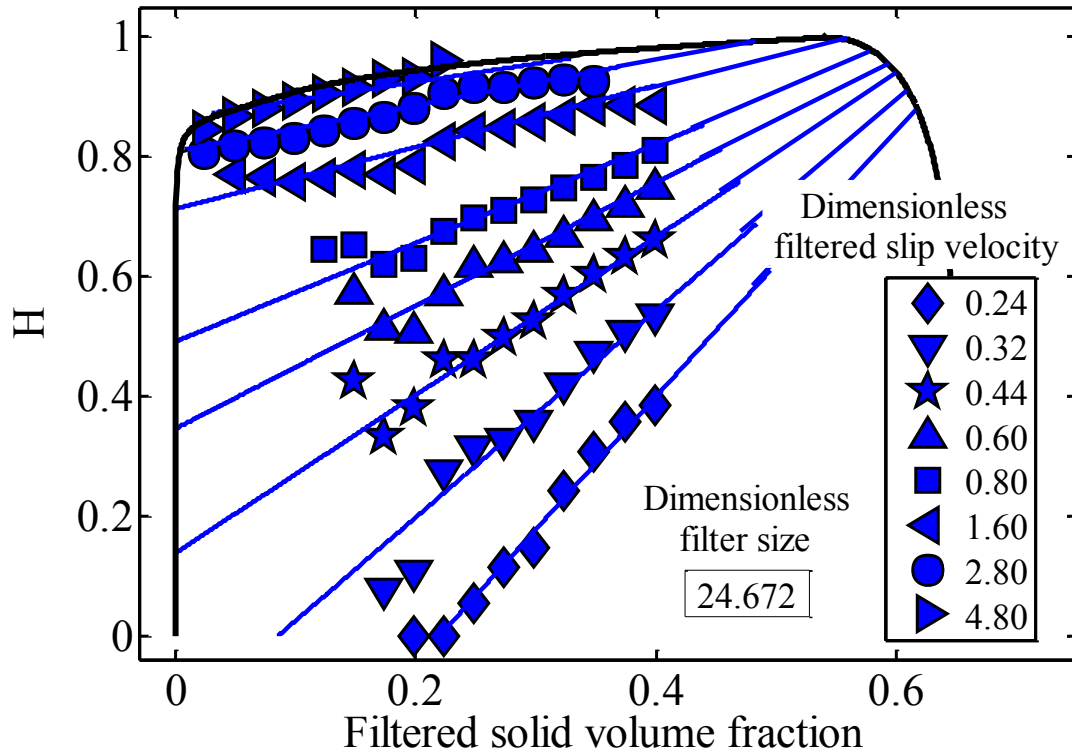
Filtered drag coefficient: The present study



- As slip velocity increases, the filtered drag coefficient decreases.
- Same trend at different filter sizes.

$$H = f \left(\frac{g\Delta_{fil}}{v_t^2}, \phi_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{v_t} \right) \left\{ \begin{array}{l} 75\mu\text{m FCC particles} \\ \text{ambient air} \end{array} \right\} \quad \frac{g\Delta_{fil}}{v_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1\text{cm}$$

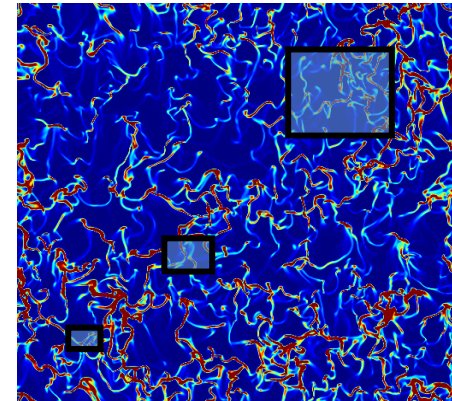
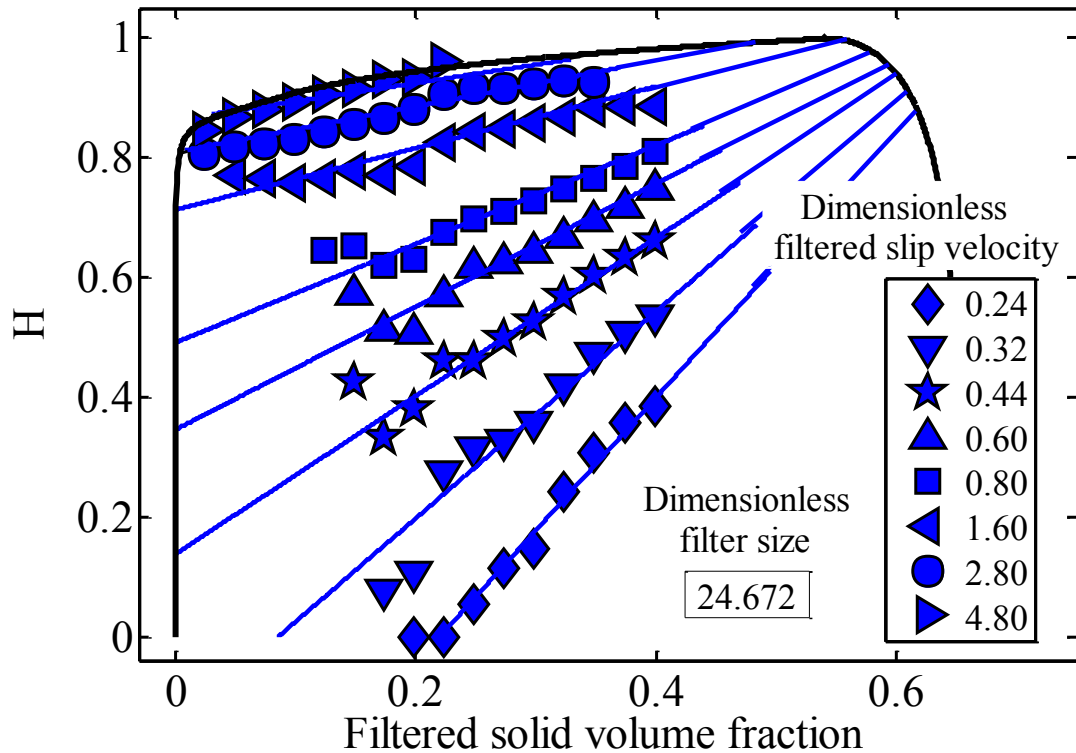
Filtered drag coefficient: The present study



- As slip velocity increases, the filtered drag coefficient decreases.
- **NOT THE USUAL INERTIAL CORRECTION!**

$$H = f\left(\frac{g\Delta_{fil}}{V_t^2}, \phi_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{V_t}\right) \left\{ \begin{array}{l} 75\mu\text{m FCC particles} \\ \text{ambient air} \end{array} \right\} \quad \frac{g\Delta_{fil}}{V_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1\text{cm}$$

Filtered drag coefficient: The present study

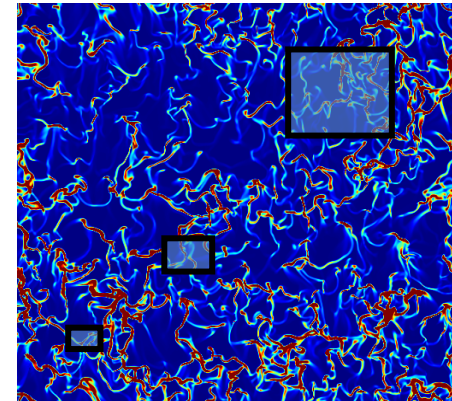
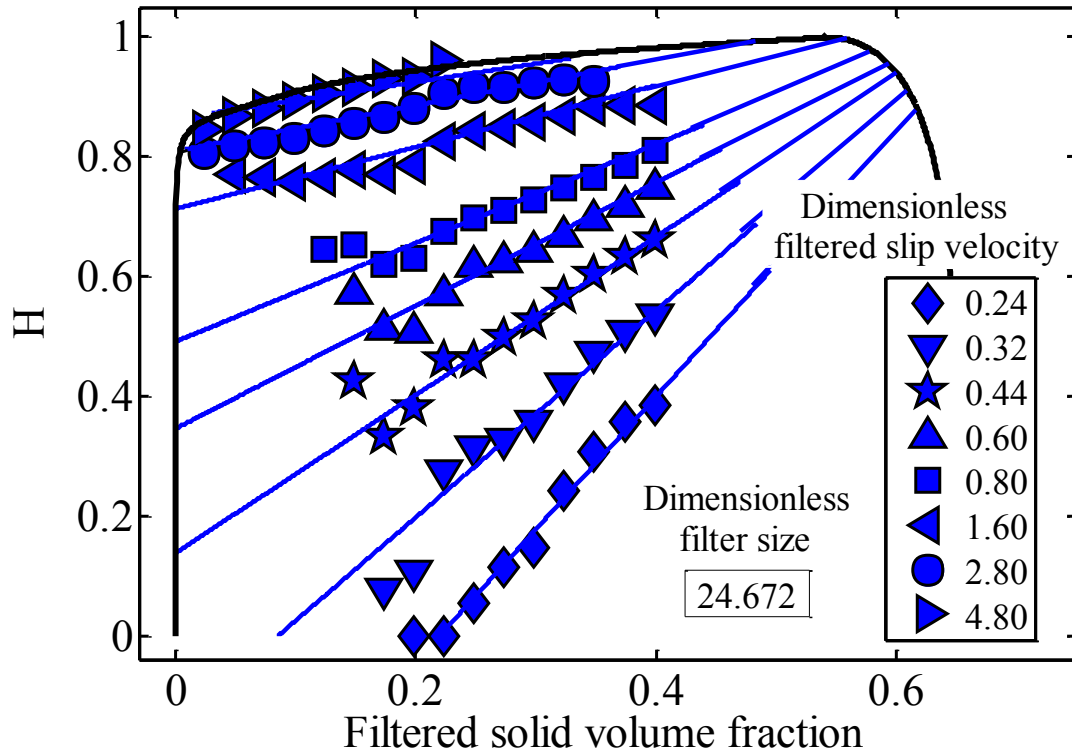


As the slip velocity increases, the sub-filter scale distribution of particles becomes more segregated

$$H = f \left(\frac{g\Delta_{fil}}{v_t^2}, \phi_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{v_t} \right) \left\{ \begin{array}{l} 75\mu\text{m FCC particles} \\ \text{ambient air} \end{array} \right\}$$

$$\frac{g\Delta_{fil}}{v_t^2} = 2.056 \Rightarrow \Delta_{fil} = 1\text{cm}$$

Filtered drag coefficient: The present study



At low slip velocities:

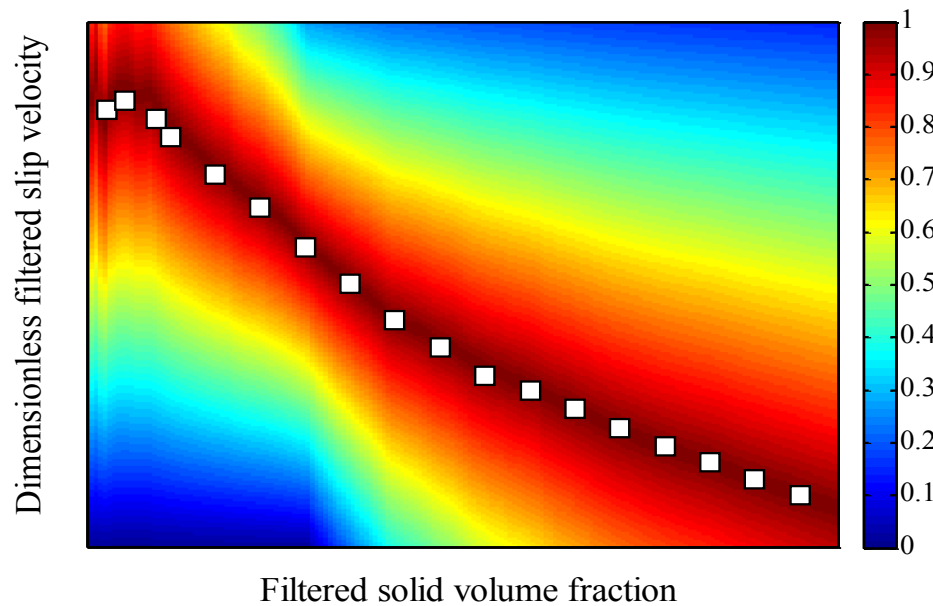
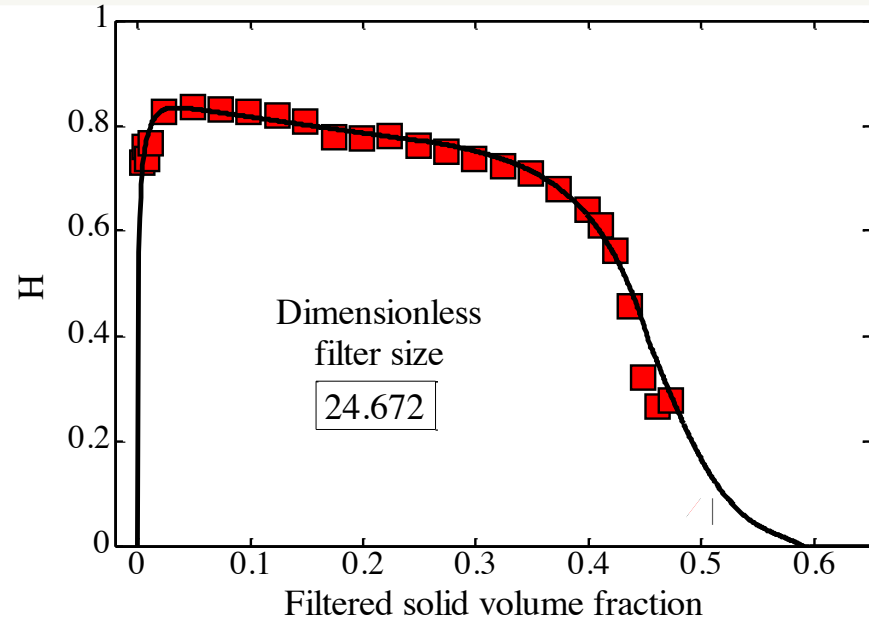
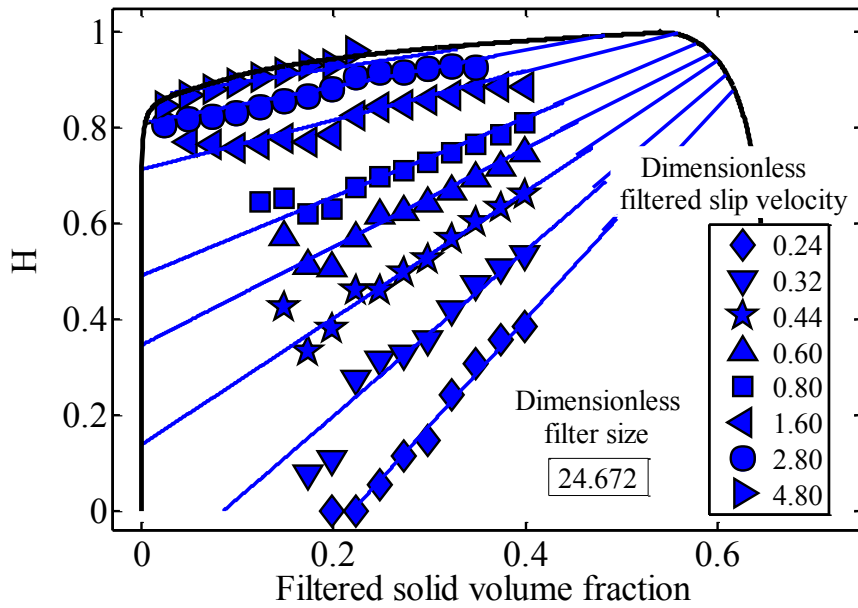
$$H_1 = \begin{cases} 0, & \overline{\phi}_s < \overline{\phi}_s^c \\ A(\overline{\phi}_s - \overline{\phi}_s^c), & \overline{\phi}_s > \overline{\phi}_s^c \end{cases}$$

At high slip velocities:

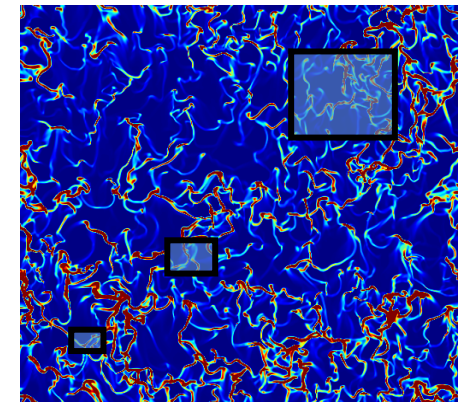
$$H_1 = B + A\overline{\phi}_s$$

$$H = \min(h_{env}, H_1)$$

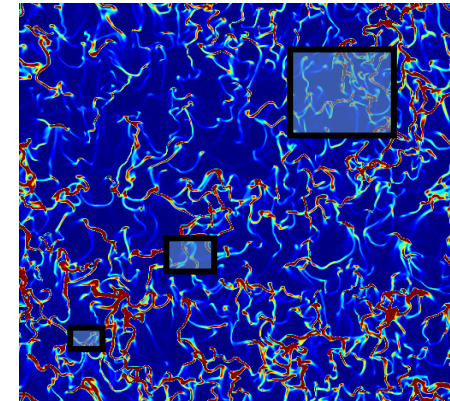
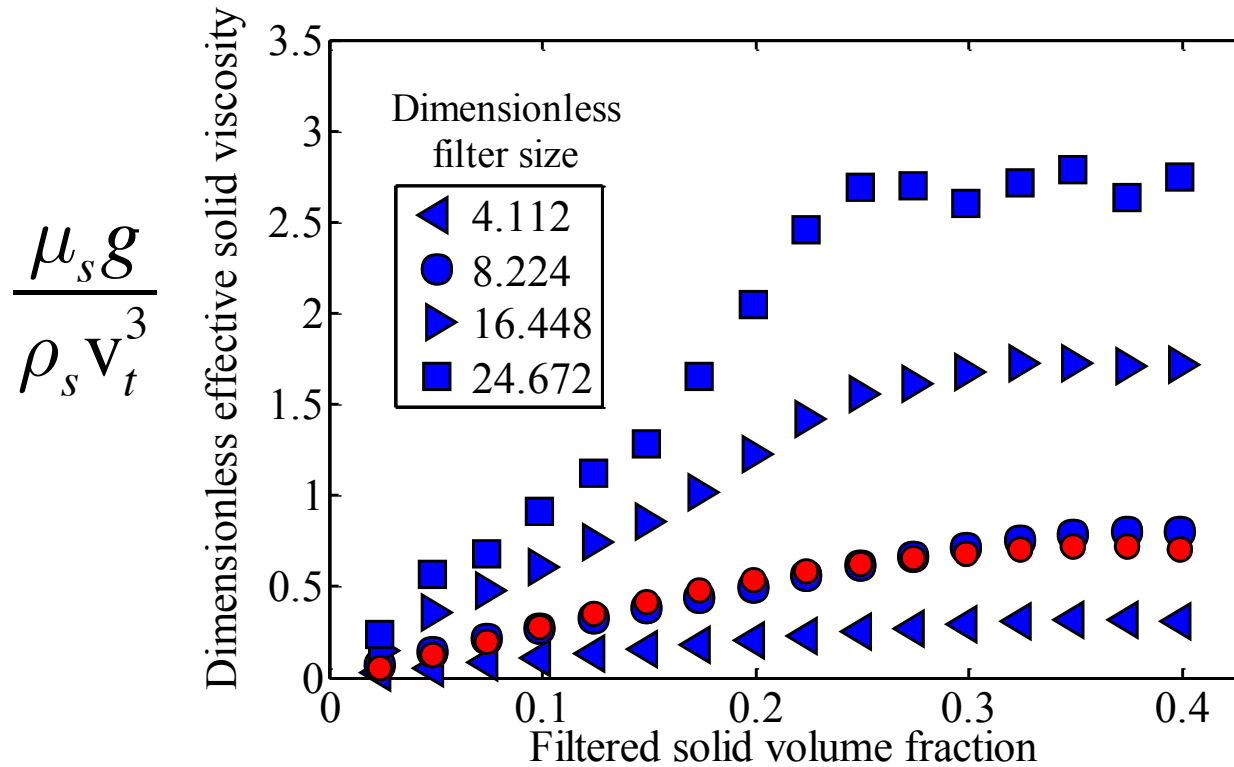
Filtered drag coefficient: The present study



$$H = f \left(\frac{g \Delta_{fil}}{v_t^2}, \bar{\phi}_s, \frac{|\tilde{\mathbf{v}}_g - \tilde{\mathbf{v}}_s|}{v_t} \right)$$



Filtered particle phase viscosity



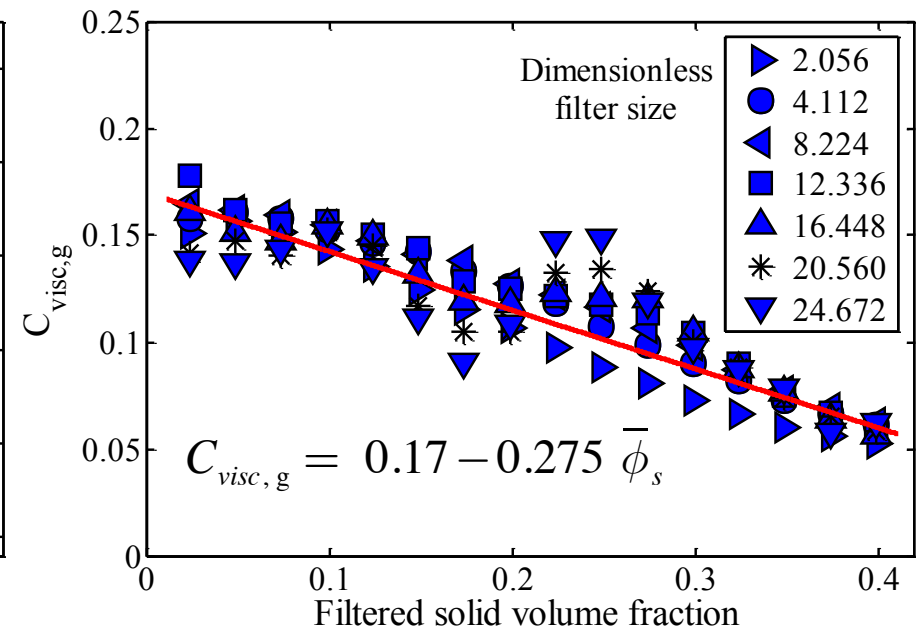
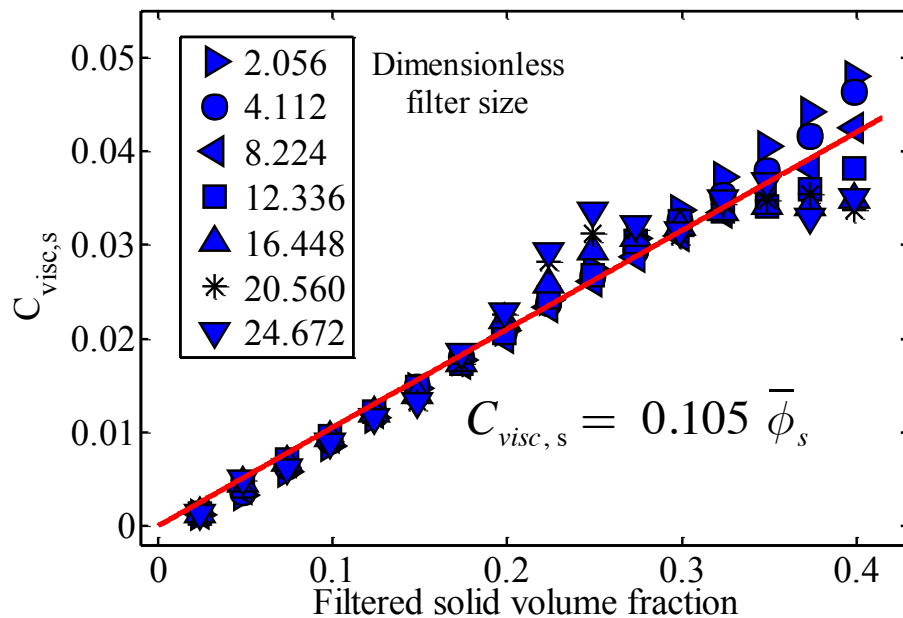
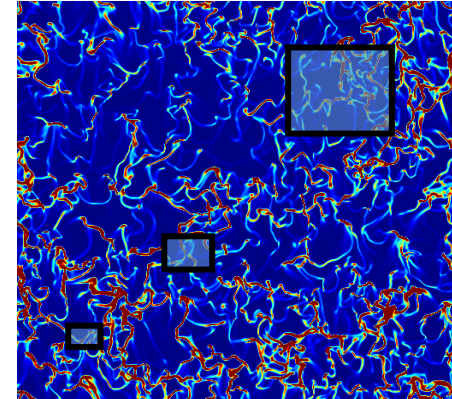
$$\frac{\mu_s g}{\rho_s V_t^3} = f\left(\frac{g \Delta_{fil}}{V_t^2}, \phi_s\right) \left\{ \begin{array}{l} 75 \mu m \text{ FCC particles} \\ \text{ambient air} \end{array} \right\} \quad \frac{g \Delta_{fil}}{V_t^2} = 4.112 \Rightarrow \Delta_{fil} = 2 cm$$

Filtered particle phase viscosity: Present study



$$\bar{S}_i = \sqrt{2\bar{S}_i : \bar{S}_i}, \quad \bar{S}_i = \frac{1}{2}(\nabla \tilde{\mathbf{v}}_i + \nabla \tilde{\mathbf{v}}_i^T) - \frac{1}{3}(\nabla \cdot \tilde{\mathbf{v}})\mathbf{I}, \quad i = s, g$$

$$\mu_{fil, i} = \rho_i \Delta_{fil}^2 \bar{S}_i C_{visc, i}, \quad i = s, g$$



Summary



- A more refined model for the filtered fluid-particle drag force is presented.
- Smagorinsky-like model for the filtered particle and fluid phase viscosities capture the computationally generated data nicely.
- Smagorinsky-like model for the meso-scale particle and fluid phase pressures (akin to turbulent kinetic energy) works nicely as well (not presented).

Acknowledgments



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Disclaimer

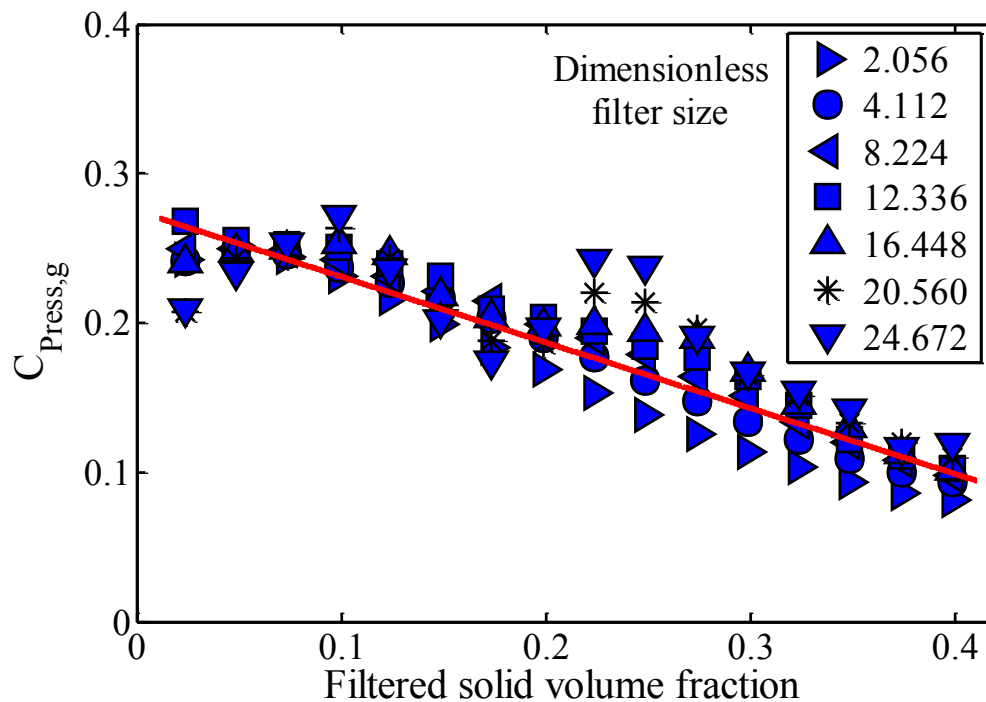
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Filtered meso-scale pressure: Present study



$$\bar{S}_i = \sqrt{2\bar{S}_i : \bar{S}_i}, \quad \bar{S}_i = \frac{1}{2}(\nabla \tilde{\mathbf{v}}_i + \nabla \tilde{\mathbf{v}}_i^T) - \frac{1}{3}(\nabla \cdot \tilde{\mathbf{v}})\mathbf{I}, \quad i = s, g$$

$$P_{fil, i} = \rho_i \Delta_{fil}^2 \bar{S}_i^2 \left(\frac{g \Delta_{fil}}{V_t^2} \right)^{2/7} C_{press, i}, \quad i = s, g$$



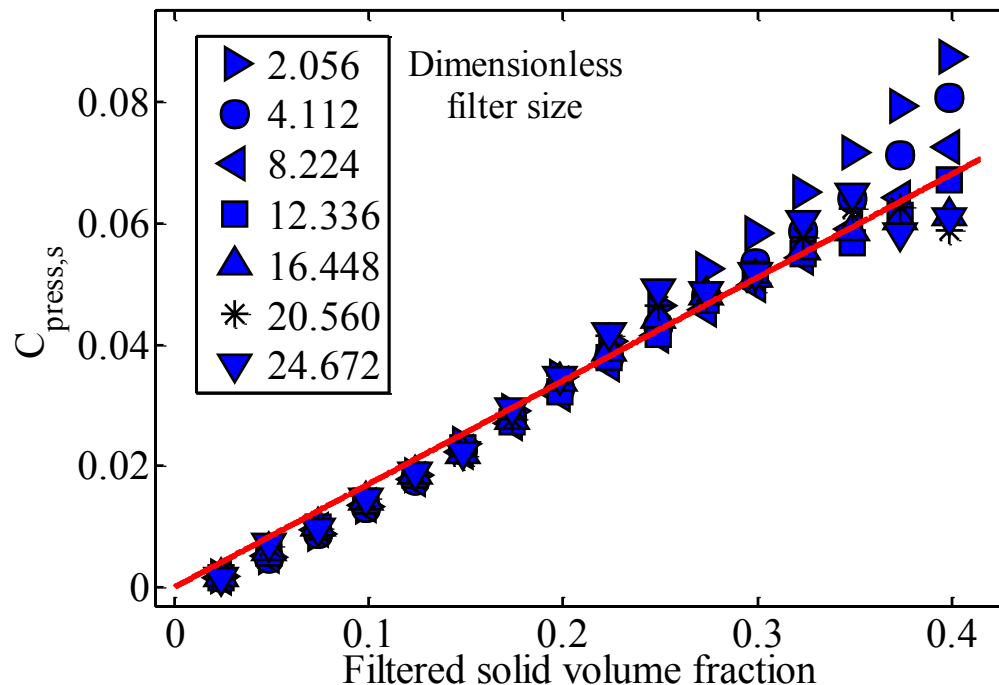
$$C_{press, g} = 0.275 - 0.44 \bar{\phi}_s$$

Filtered meso-scale pressure: Present study



$$\bar{S}_i = \sqrt{2\bar{\mathbf{S}}_i : \bar{\mathbf{S}}_i}, \quad \bar{\mathbf{S}}_i = \frac{1}{2}(\nabla \tilde{\mathbf{v}}_i + \nabla \tilde{\mathbf{v}}_i^T) - \frac{1}{3}(\nabla \cdot \tilde{\mathbf{v}})\mathbf{I}, \quad i = s, g$$

$$P_{fil, i} = \rho_i \Delta_{fil}^2 \bar{S}_i^2 \left(\frac{g \Delta_{fil}}{V_t^2} \right)^{2/7} C_{press, i}, \quad i = s, g$$



$$C_{press, s} = 0.17 \bar{\phi}_s$$