

Integration of High-Fidelity CO₂ Sorbent Models at the Process Scale Using Dynamic Discrepancy

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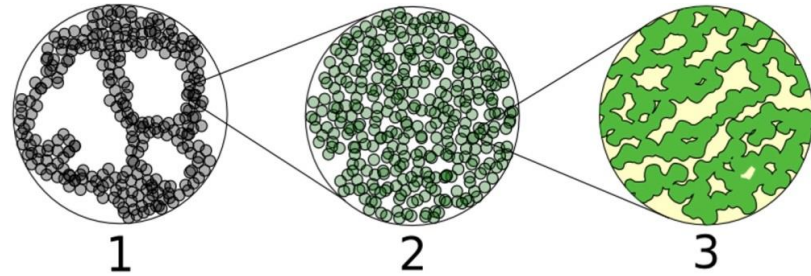
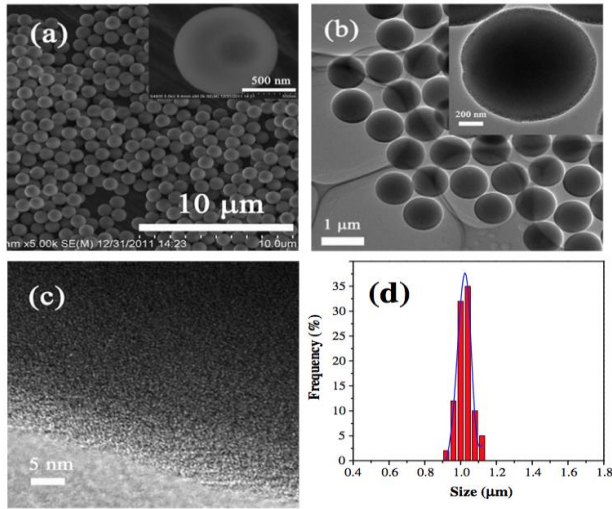
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Overview

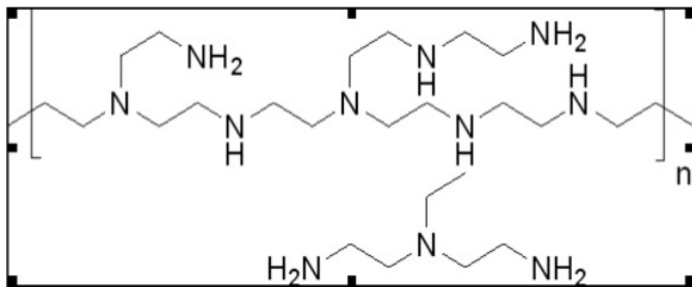
- Introduction: PEI adsorbents and reaction kinetics
- Motivation and new mechanism
- Dynamic discrepancy reduced model and Bayesian calibration
- Conclusions and future work

Introduction: Amine-based Adsorbents



Length scale: (1) macroporosity
 (2) meso-porous particles
 (3) Silica-PEI composite

SEM (a), TEM (b), HRTEM (c) images and particle-size distribution histogram (d) of the S600-10 sample



PEI structure

Mass transport:

Gas phase diffusion in mesopores;

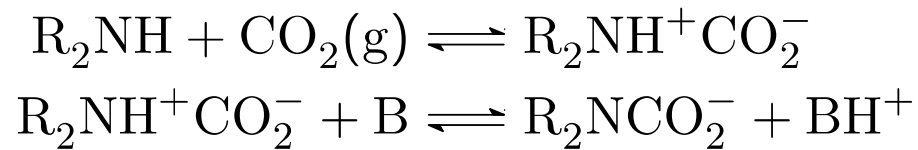
Solid state diffusion in silica-PEI composites.

Yao, L., et al., Journal of colloid and interface science 408 (2013): 173-180
 Mebane, D.S., et al., The Journal of Physical Chemistry C 117.50 (2013): 26617-26627.

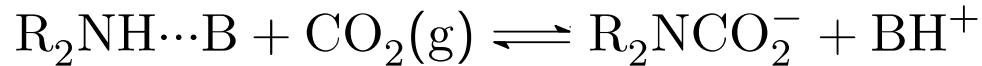


Introduction: Reaction Kinetics

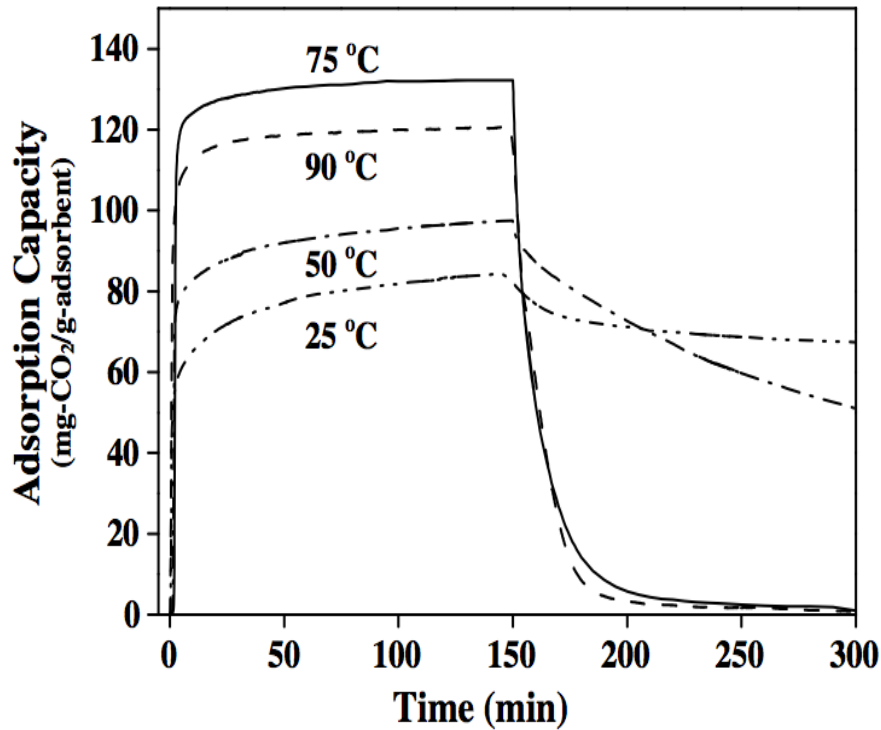
- Zwitterion Mechanism



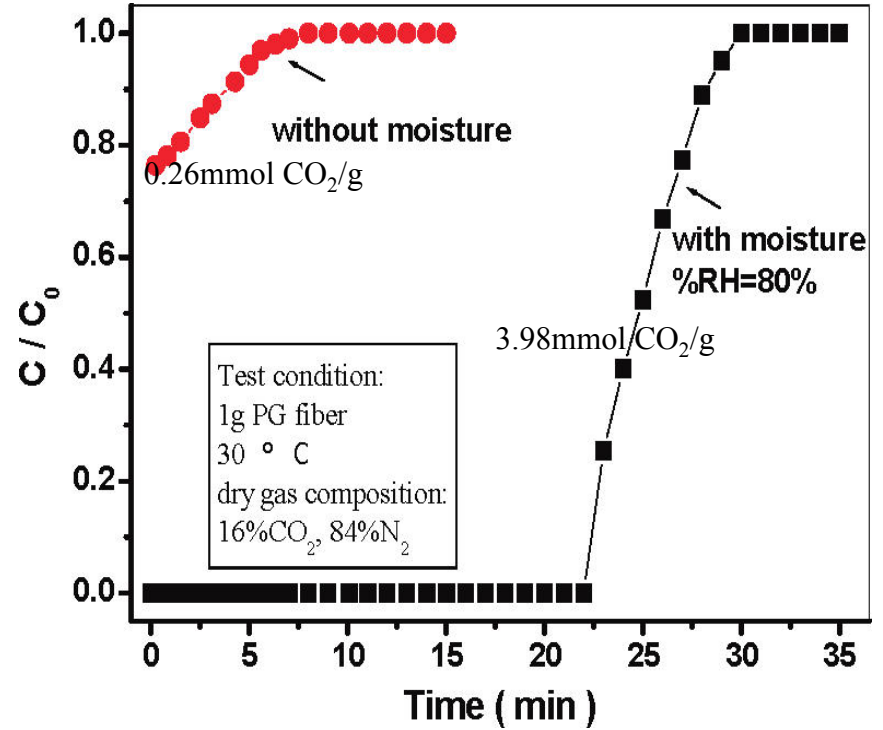
- Termolecular Mechanism



Motivation



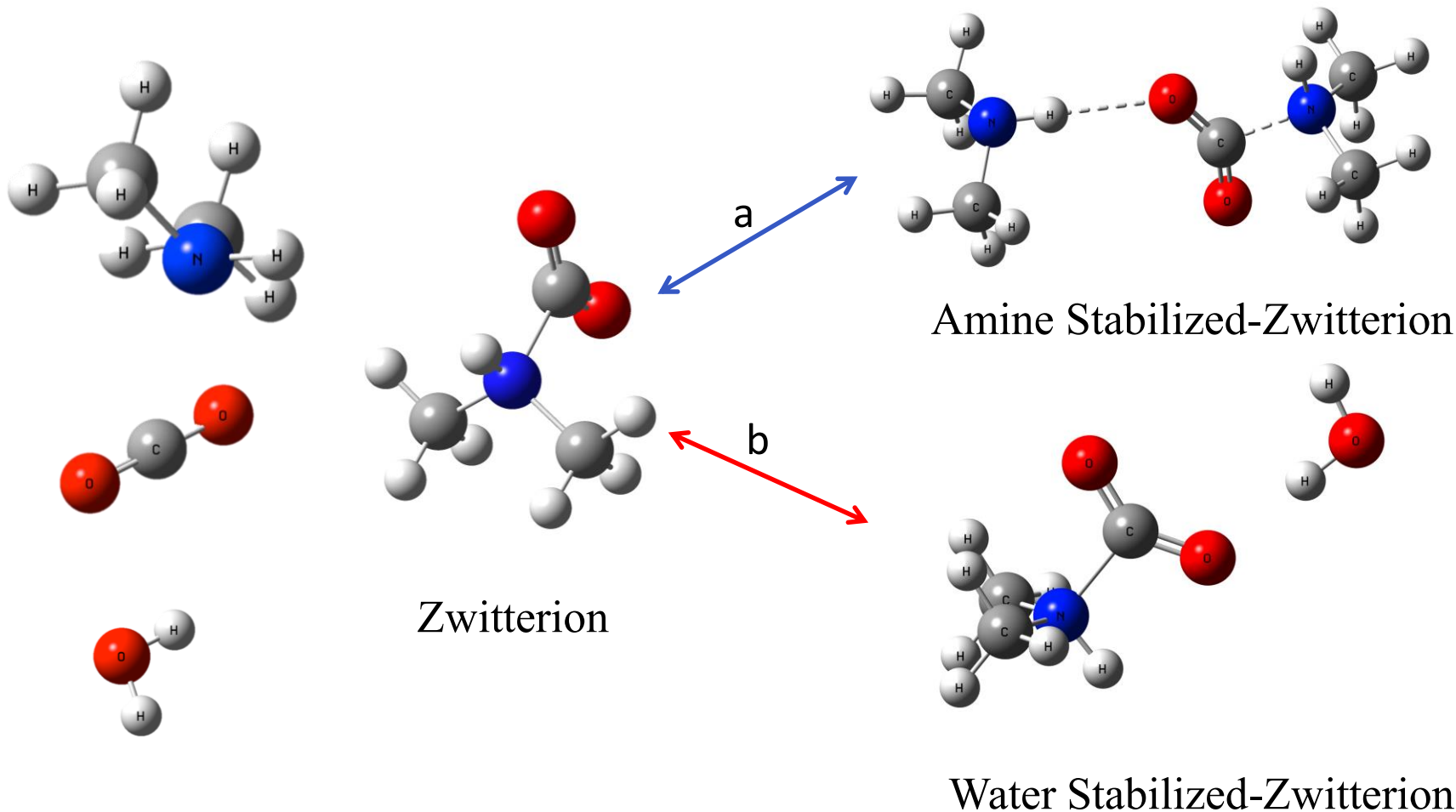
The effect of temperature on the CO₂ adsorption–desorption performance of KIT-6-PEI 50



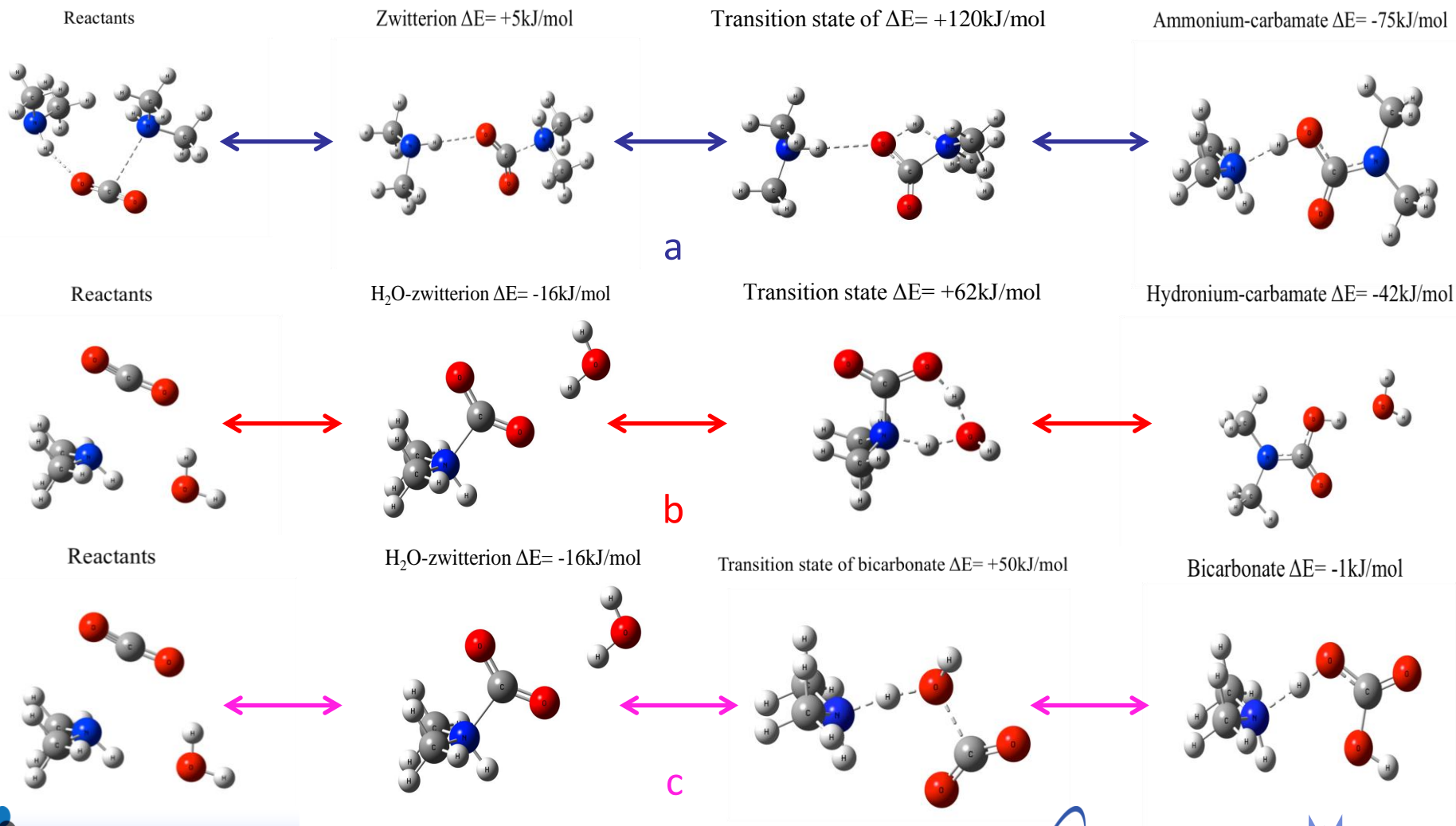
Comparison of the adsorbed volume of CO₂ from simulated dry and moist flue gas.

W.J. Son et al., Microporous and Mesoporous Materials 113 (2008) 31–40 Li, P., et al., Langmuir, 2008, 24 (13): 6567-6574

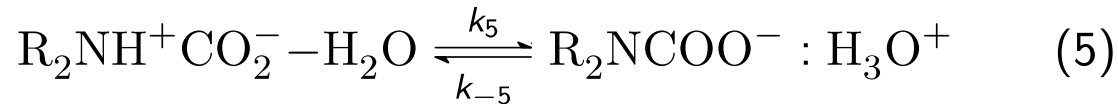
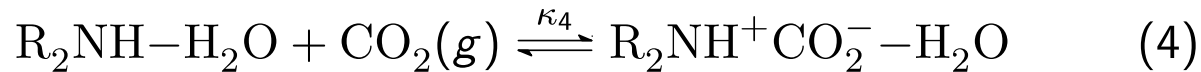
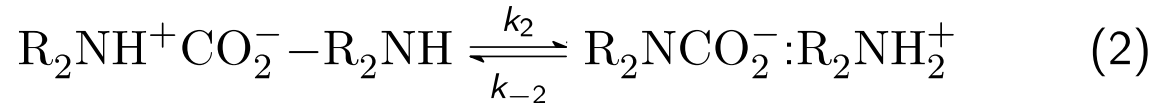
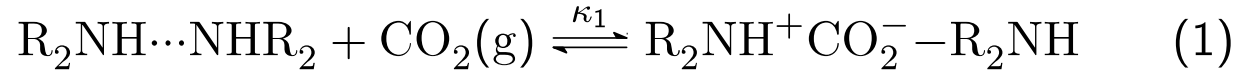
New Mechanism



New Mechanism



New Mechanism



Variables: $z_1 = \text{Amine-Zw (1)}$ $x = \text{Ammonium-Carbamate (2)}$

$z_2 = \text{Amine-H}_2\text{O (3)}$ $z_3 = \text{H}_2\text{O-Zw (4)}$

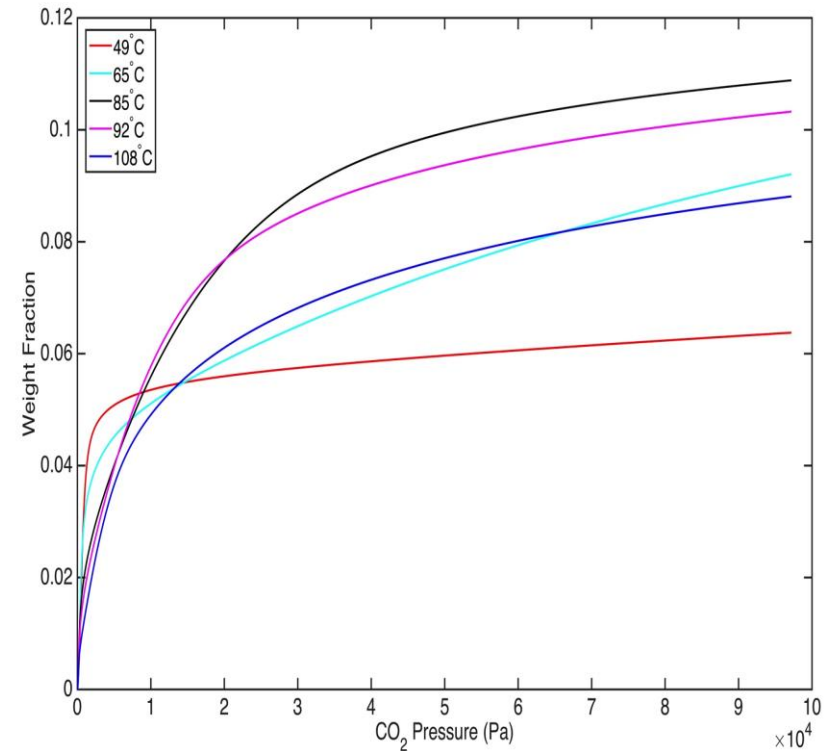
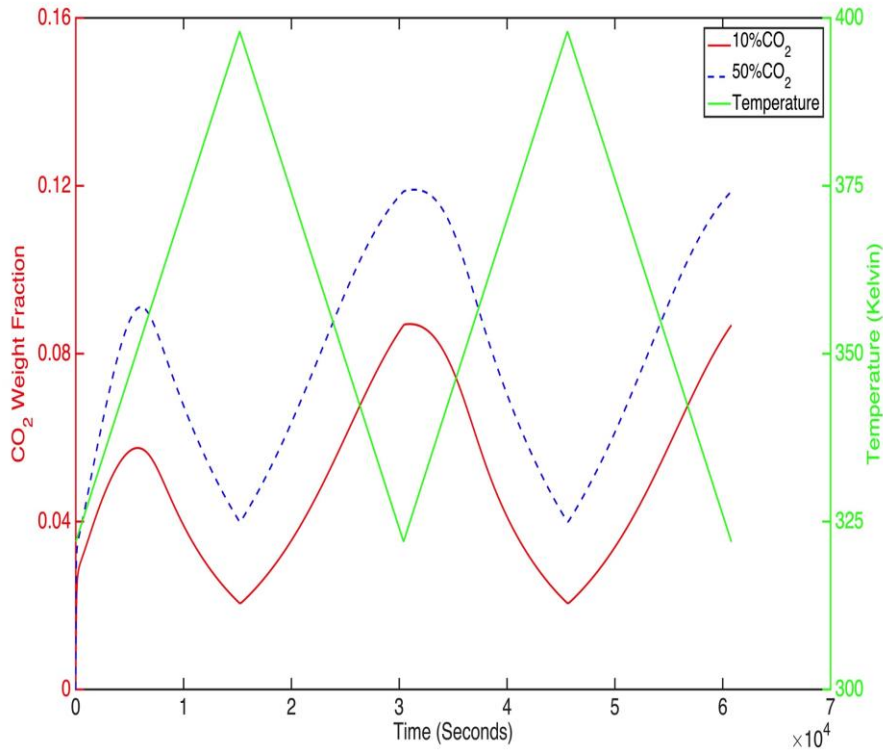
$y = \text{Hydronium-Carbamate (5)}$

Solutions:

$$W_{CO_2} = M_{CO_2} n_v (x + y + z_1 + z_3) / \rho$$

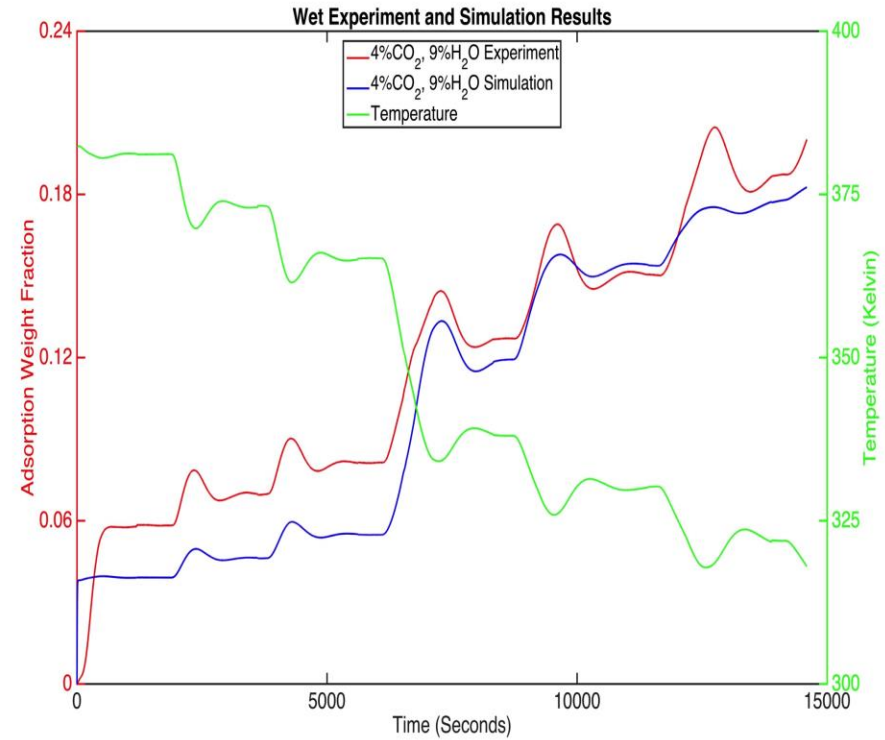
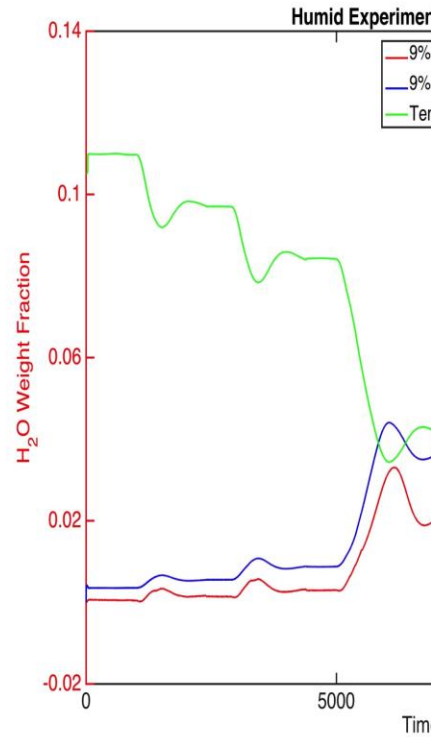
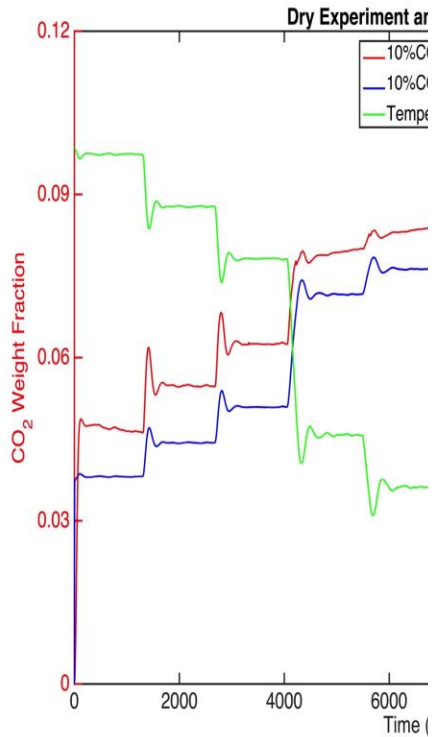
$$W_{H_2O} = M_{H_2O} n_v (y + z_2 + z_3) / \rho$$

Simulation Results on Temperature Effect





Experiment and Simulation Results



Methods: Bayesian Calibration and Dynamic Discrepancy

Bayesian Calibration:

$$\mathcal{P}(A|B) = \frac{\mathcal{P}(B|A)\mathcal{P}(A)}{\int_{A'} \mathcal{P}(B|A')dA'}$$

$$\mathcal{Z} = Y(\theta) + \delta(\xi) + \epsilon(\psi)$$

$$\Omega(\theta, \xi, \psi|Z) \propto \mathcal{L}(Z|\theta, \xi, \psi)\pi(\theta, \xi, \psi)$$

Dynamic Discrepancy:

Discrepancy on Kinetic non-ideality :

$$u_{b_i}^* = \zeta_b \exp\left(\frac{-\Delta H_b^\ddagger}{RT}\right)$$

$$u_{b_i, new}^* = \zeta_b \exp\left(\frac{-\Delta H_b^\ddagger}{RT}\right) \exp\left[\delta(z_{i-1}, z_i, z_{i+1}, \frac{1}{T})\right] / T$$

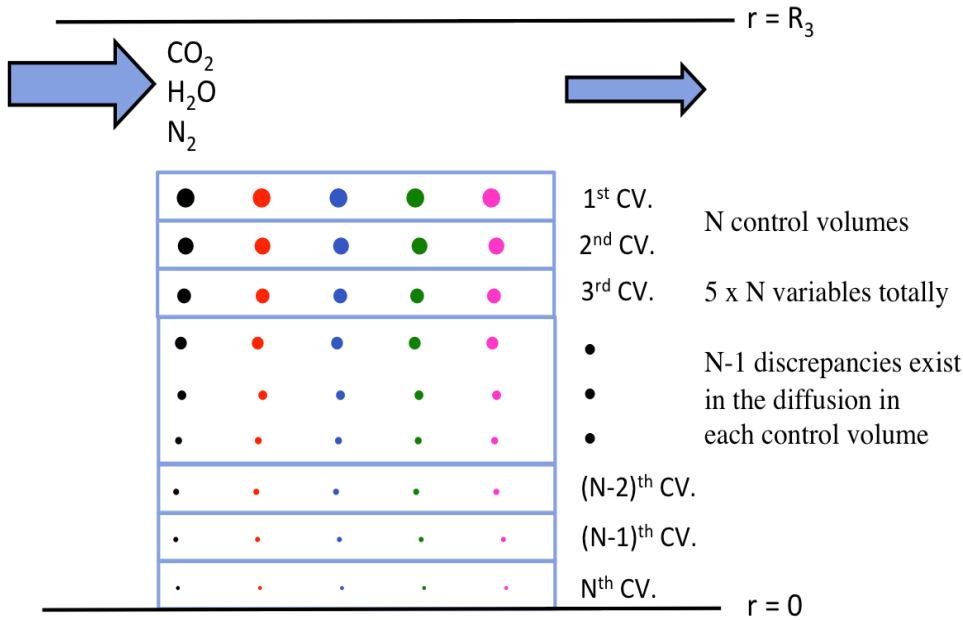
$$= u_{b_i}^* \exp\left[\delta(z_{i-1}, z_i, z_{i+1}, \frac{1}{T})\right]$$

Discrepancy on Thermodynamic Equilibrium :

$$\kappa = \exp\left(\frac{-\Delta H + T\Delta S}{RT}\right) / P$$

$$\kappa_{new} = \kappa * \exp[\delta^E(P, T)]$$

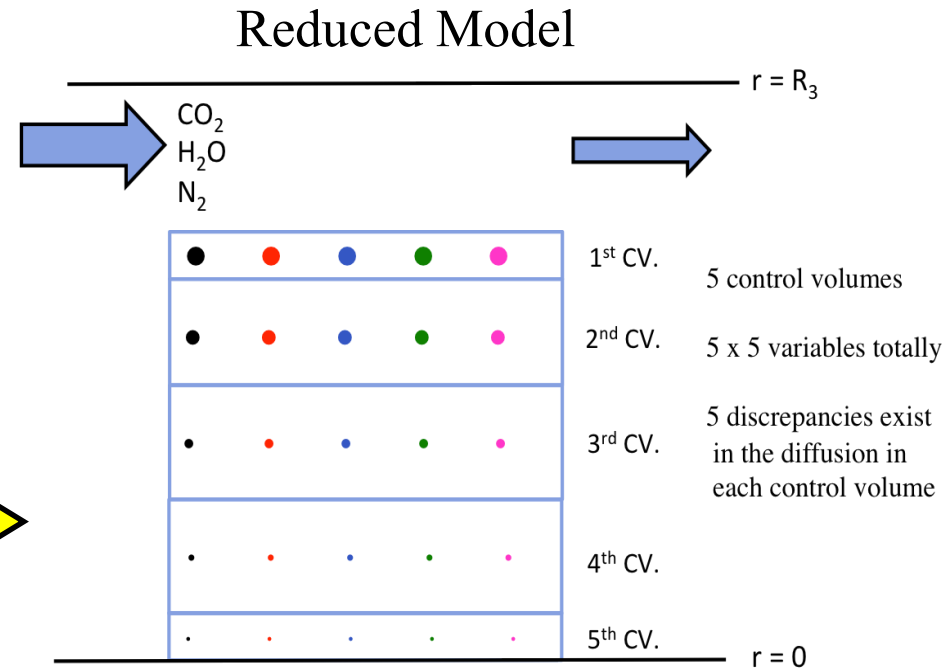
Reduced Model



Normal Model

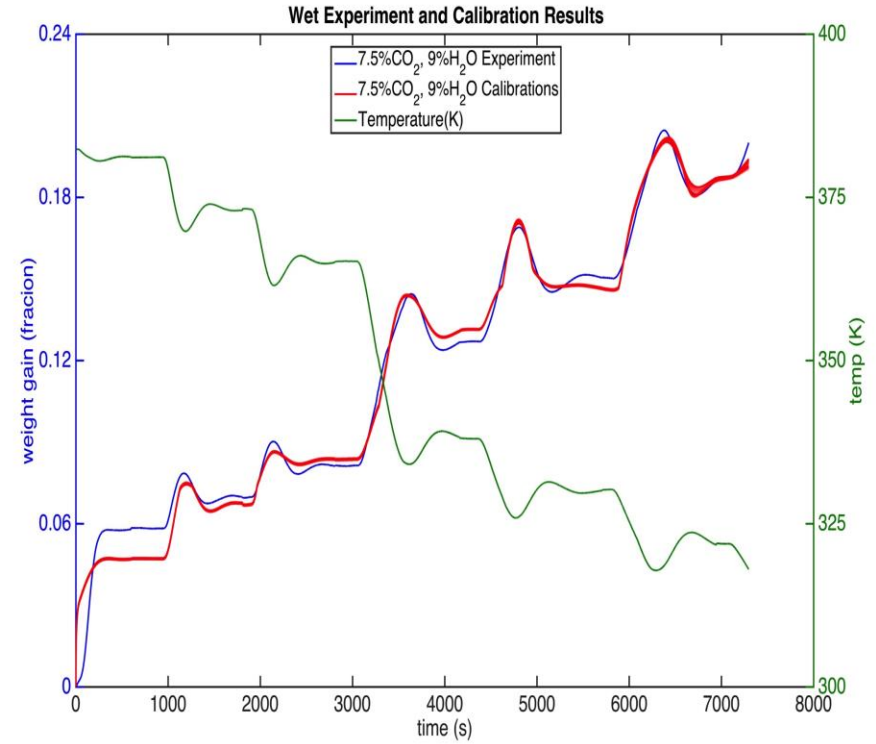
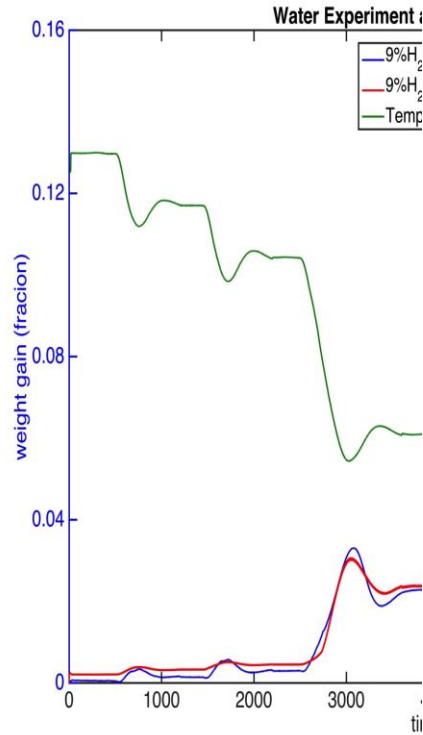
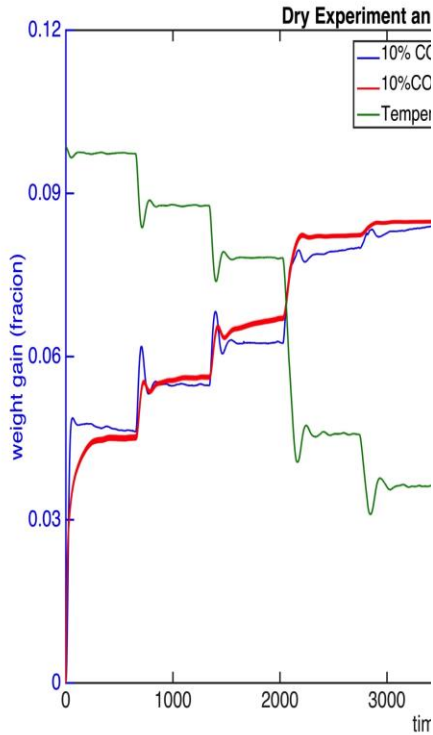


Increase the calculation speed by reducing the control volumes and add discrepancy to diffusivity coefficients



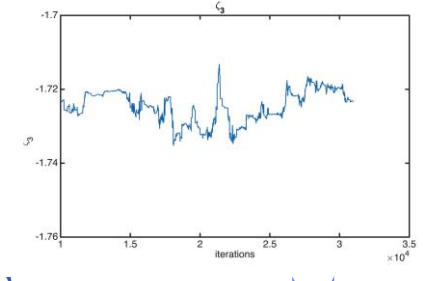
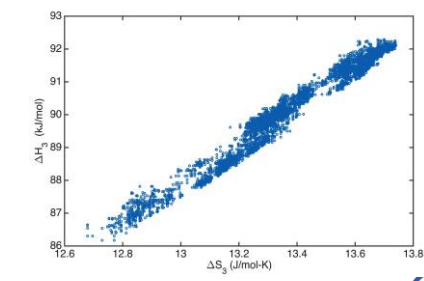
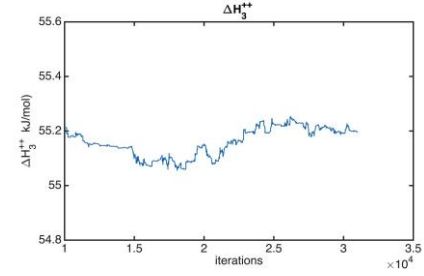
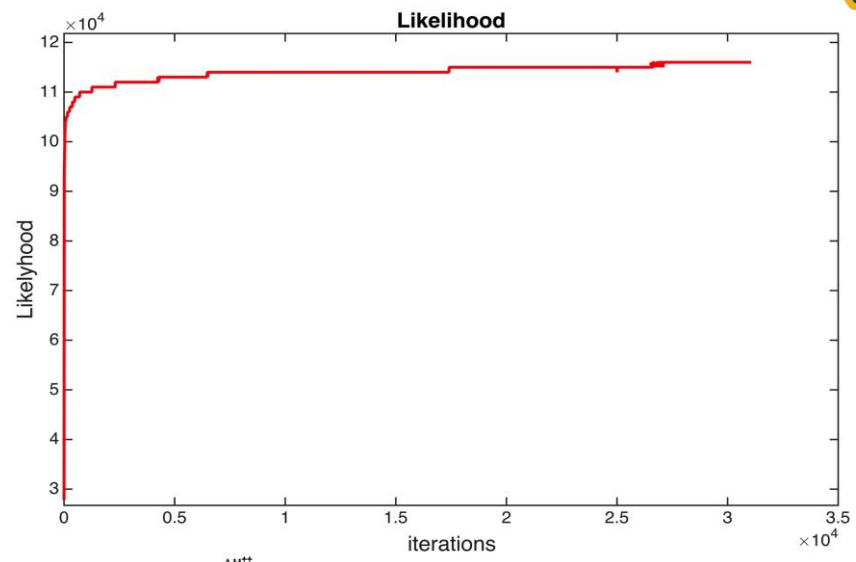
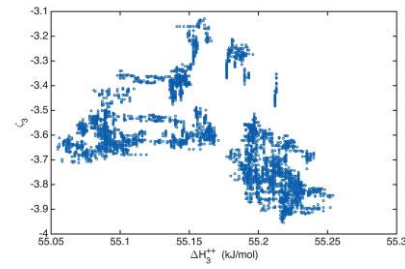
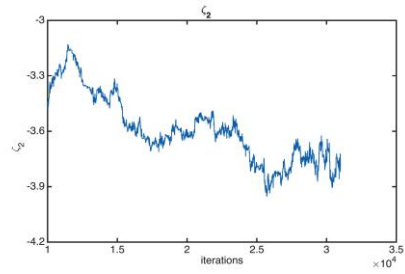
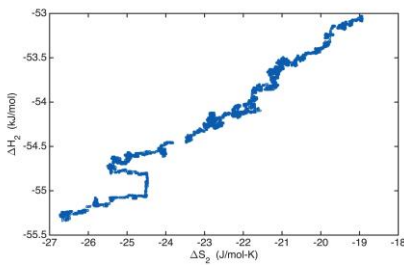
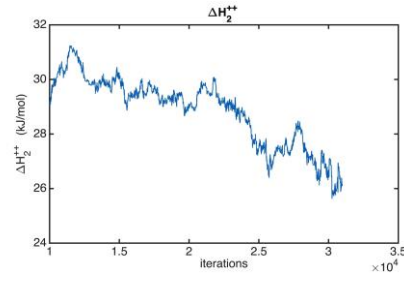
Reduced Model

Calibration Results





Calibration Results





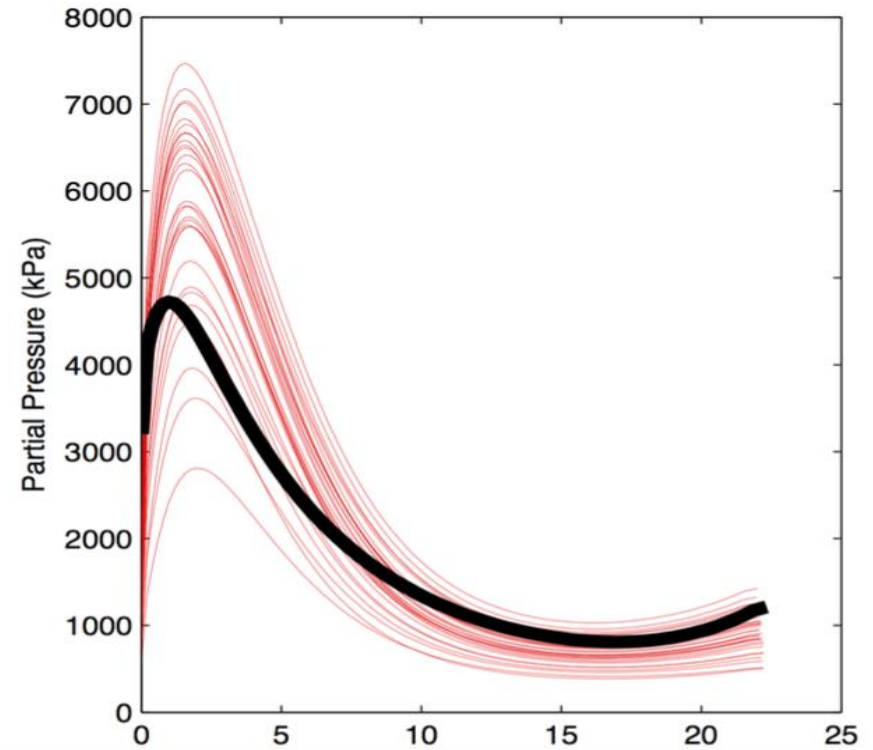
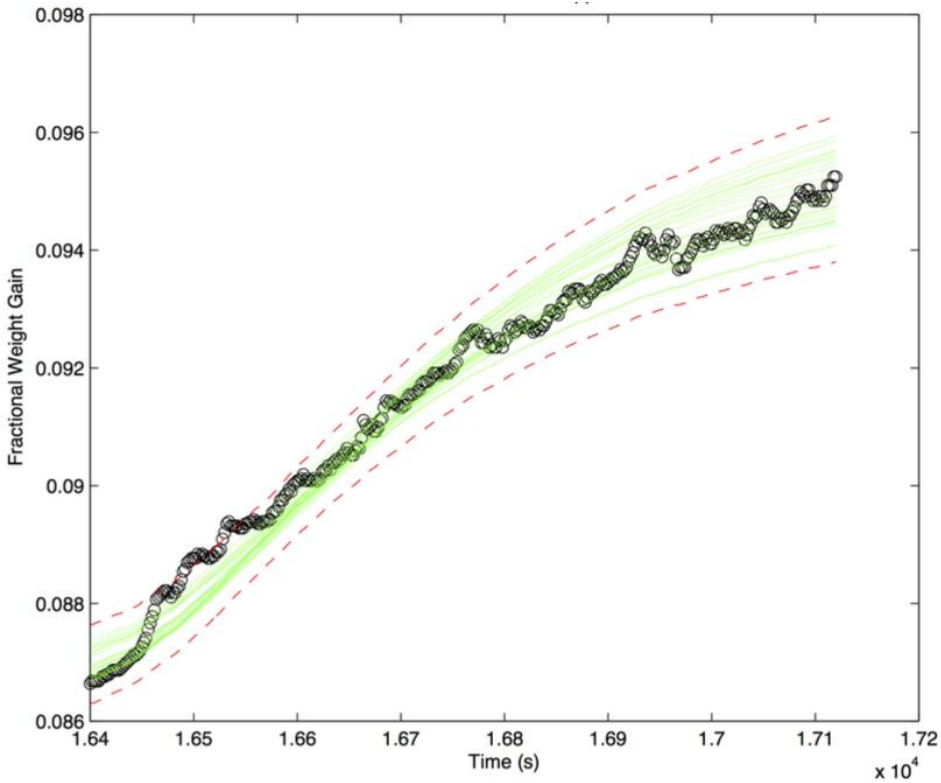
Conclusion

- A new mechanism using amine and water stabilized zwitterions as diffusive intermediates has been proposed
- Model simulation replicated the experiment results qualitatively
- Bayesian calibration and dynamic discrepancy implemented in the model to get quantitatively matched results
- Reduced model is used to improve the calculation speed

Future Work

- Apply this model to bubbling fluidized bed model
- Quantify the uncertainty from model reduction and model upscaling

Upscaling Results



Bhat, K.S., et al., arXiv preprint arXiv:1411.2578 (2014).



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