

New Diffusive Intermediates for CO₂ Adsorption in Silica-Supported Amine Sorbents

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Overview

Sorbents, multi-scale model

Two step zwitterion mechanism

Water stabilized zwitterion mechanism

Conclusions and future work







Sorbents

Sorbents: Silica support with PEI loading



SEM (a), TEM (b), and HRTEM (c) images and particle-size distribution histogram (d) of the S600-10 sample

Heydari-Gorji A, et al., Energy & Fuels, 2011, 25(9): 4206-4210.





PEI structure





Multi-scale model



Length scale: (1) macroporosity (2)meso-porous particles (3) Silica-PEI composite

Mass transport:

Gas phase diffusion in mesopores; Solid state diffusion in silica-PEI composites.

DS Mebane, et al., The Journal of Physical Chemistry C 117.50 (2013): 26617-26627.







Temperature effect on adsorption capacity



The effect of temperature on the CO₂ adsorption–desorption performance of KIT-6-PEI 50 (150 min adsorption, 150 min desorption)

W.J. Son et al., Microporous and Mesoporous Materials 113 (2008) 31-40







Zwitterion mechanism





Sensitivity analysis



Total variance indices for all parameters plotted at 4%

 $\rm CO_2$

DS Mebane, et al., The Journal of Physical Chemistry C 117.50 (2013): 26617-26627.





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Role of water in CO₂ adsorption



Flow rate effects on adsorption capacity in uncooled, non-prehydrated fibers vs. prehy- drated fibers

Y Fan, et al., AIChE Journal, 2014, 60(11): 3878-3887.



Comparison of the adsorbed volume of CO2 from simulated dry and moist flue gas.

P Li, et al., Langmuir, 2008, 24 (13): 6567-6574



TGA experiment results



- EST.1943



Water effect on stabilizing zwitterion









∆E=+5kJ/mol Zwitterion

 $\Delta E=-18$ kJ/mol $\Delta E=-36$ kJ/mol Stabilized zwitterions

Reactants

DS Mebane, et al., The Journal of Physical Chemistry C 117.50 (2013): 26617-26627.





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Chemical reactions with new diffusive intermediates

New zwitterion, ΔE=-18kJ/mol

Transition state, ΔE=+53kJ/mol

$$R_2NH + H_2O \stackrel{kap_1}{\longrightarrow} R_2NH - H_2O$$
 (1)

$$R_2 NH - H_2 O + CO_2 \xrightarrow{kap_2} R_2 NH^+ COO^- - H_2 O$$
 (2)

$$R_2 NH + CO_2 \stackrel{kap_3}{\longleftarrow} R_2 NH^+ COO^-$$
 (3)

$$R_2 NH^+ COO^- + R_2 NH \xleftarrow{k_4}{k_{-4}} R_2 NH_2^+ : R_2 NCOO^-$$
(4)

$$R_2 NH^+ COO^- - H_2 O \xrightarrow[k_{-5}]{k_{-5}} R_2 NCOO^- : H_3 O^+$$
 (5)

Hydronium-Carbamate, $\Delta E=-34$ kJ/mol







Dry simulation Results



- EST.1943



Wet simulation Results



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EST. 1943



Conclusions and future work

- The stability of transport intermediates are important to the capacity of sorbents
- Water increases the capacity of sorbents
- Zwitterion is not stable under dry cases and can be stabilized by water
- CO₂ capacity decrease when increase the CO₂ concentration of humid flue gases

- Bayesian calibration to quantitative results
- Dynamic discrepancy for multi-scale process model







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